Collaborative Fluid Dynamics Research: Porous Media, Microfluidics, and Bio-Flows

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Overview

- Background
- Simulations
  - Flow Through Porous Media (FTPM)
  - Flow in Junctions/Microjunctions
  - Microelbows
  - Entrance Length in Microtubes
- Experimental
  - Millijunctions
  - Bio-Scaffolds
  - Renal Artery Aneurysm
  - Microtubes
- Future Directions

Applications

Flow in microfluidic flow networks and flow in porous networks are of interest in many engineering applications.

Applications include porous media, micro-power generation, biomedical, computer chips, chemical separation processes, micro-valves, micro-pumps, and micro-flow sensors

Yanuka, M., Dullien, F.A.L., and D.E. Elrick, 1986, “Percolation Processes And Porous Media I. Geometrical And Topological Model Of Porous Media Using A Three-Dimensional Joint Pore Size Distribution,” J.Colloid Interface Sci., **112**, pp. 24-41.

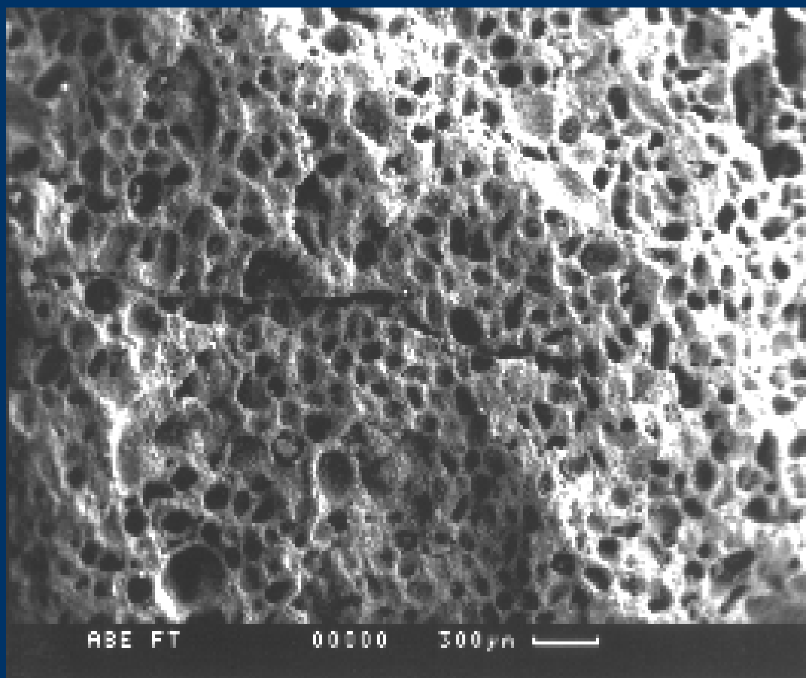
Lee, W.Y., Wong, M., and Zohar, Y., 2002, “Microchannels in Series Connected Via a Contraction/expansion Section”, J. Fluid Mech., **459**, pp.187-206.

Judy, J., Maynes, D., and Webb, B.W., 2002, “Characterization of Frictional Pressure Drop for Liquid Flows Through Microchannels,” Intl. J. Heat Mass Trans., **45**, pp.3477-3489.

Flow in these applications is usually laminar

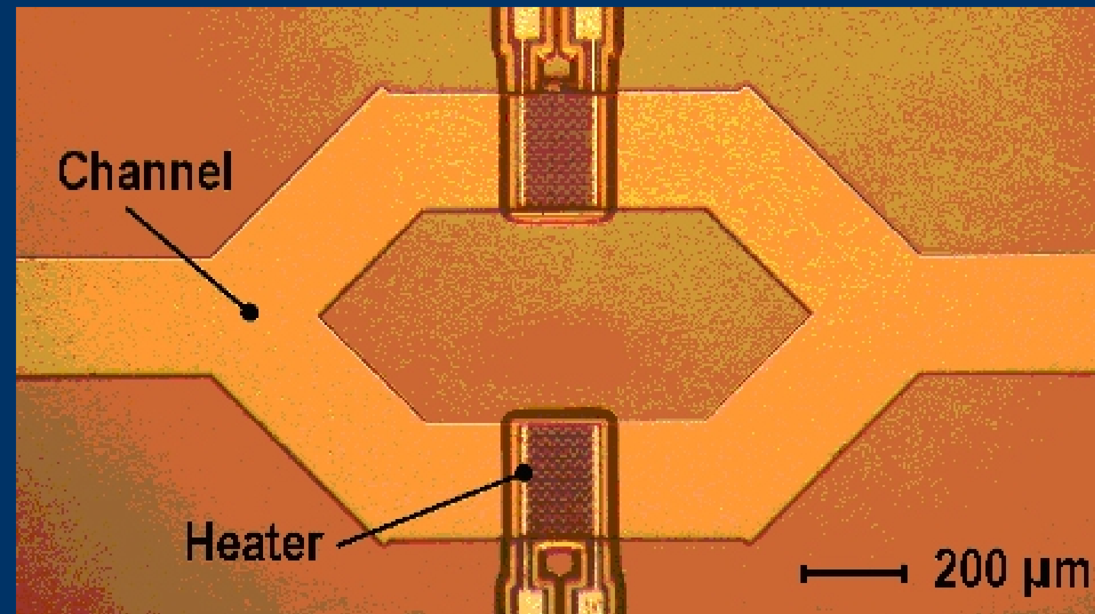
Graveson, P., Branebjerg, J., and Jensen, O.S., 1993, “Microfluidics a Review,” J. Micromech. Microeng., 3, pp.168-182.

Porous Media



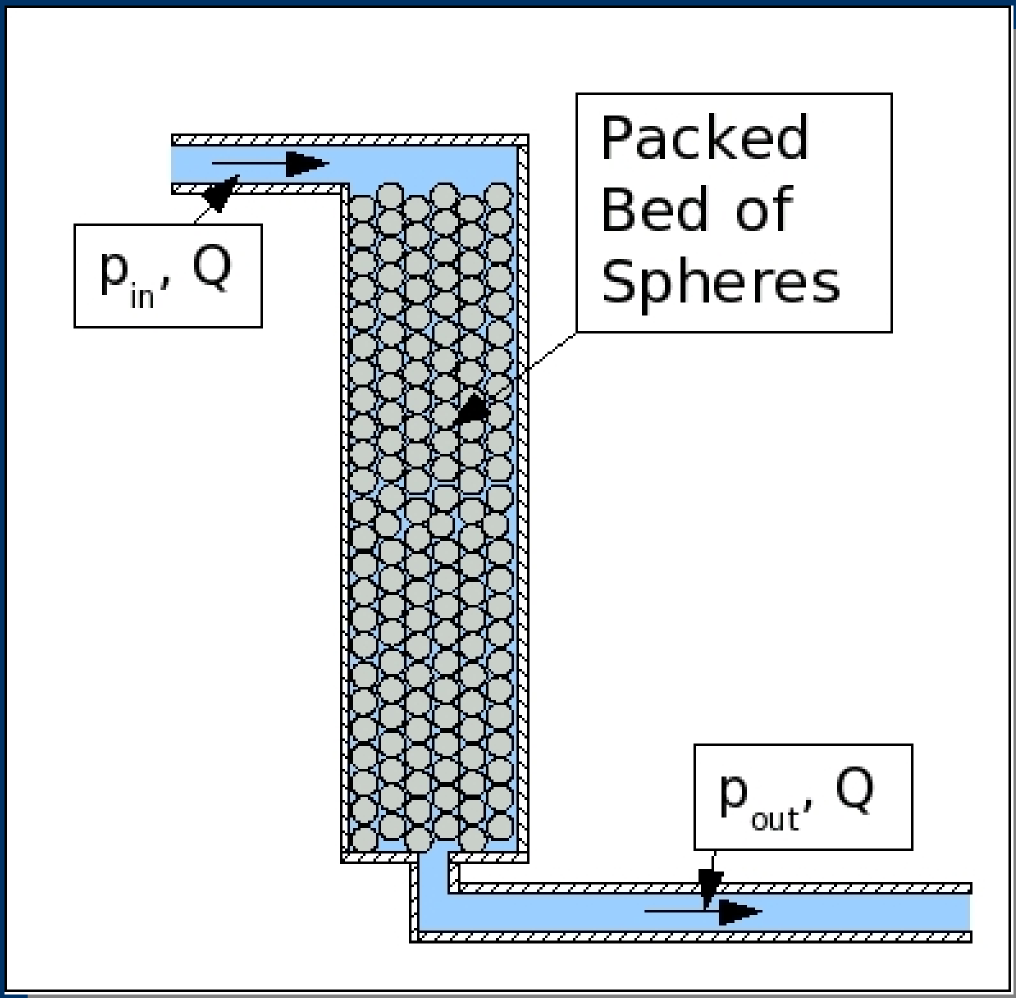
Highly porous magnesian limestone.
(www.dawntnicholson.org.uk)

Microfluidic Devices



Microfluidic Valve Structure.
(http://www.cchem.berkeley.edu/sjmgrp/people/boris/boris.htm)

Artificial Porous Media



Packed Beds, Gas and Liquid Filters

Sphere sizes 妬m to cm

Hold-up for chemical reaction, thermal processing, or filtering

Basics of Porous Media

Low Speed Flow – Darcy's Law

$$\frac{dp}{dx} = \frac{\mu}{\kappa} u$$

$p = pressure \quad x = position$

$\mu = viscosity \quad \kappa = permeability$

$u = filtration \quad velocity$

High Speed Flow – Forscheimer's Law

$$\frac{dp}{dx} = \frac{\mu}{\kappa} u + \rho \beta u^2$$

$\rho = density$

$\beta = Forccheimer's \quad Coefficient$

Packed Beds – Ergun's Equation (empirical)

$$\frac{-\Delta p}{\Delta L} = \frac{150 \mu}{d_p^2} \frac{(1-\phi)^2}{\phi^3} u + \frac{1.75 \rho (1-\phi)}{d_p \phi^3} u^2$$

$\phi = porosity$

$d_p = mean \quad sphere \quad diameter$

Flow Through Porous Media

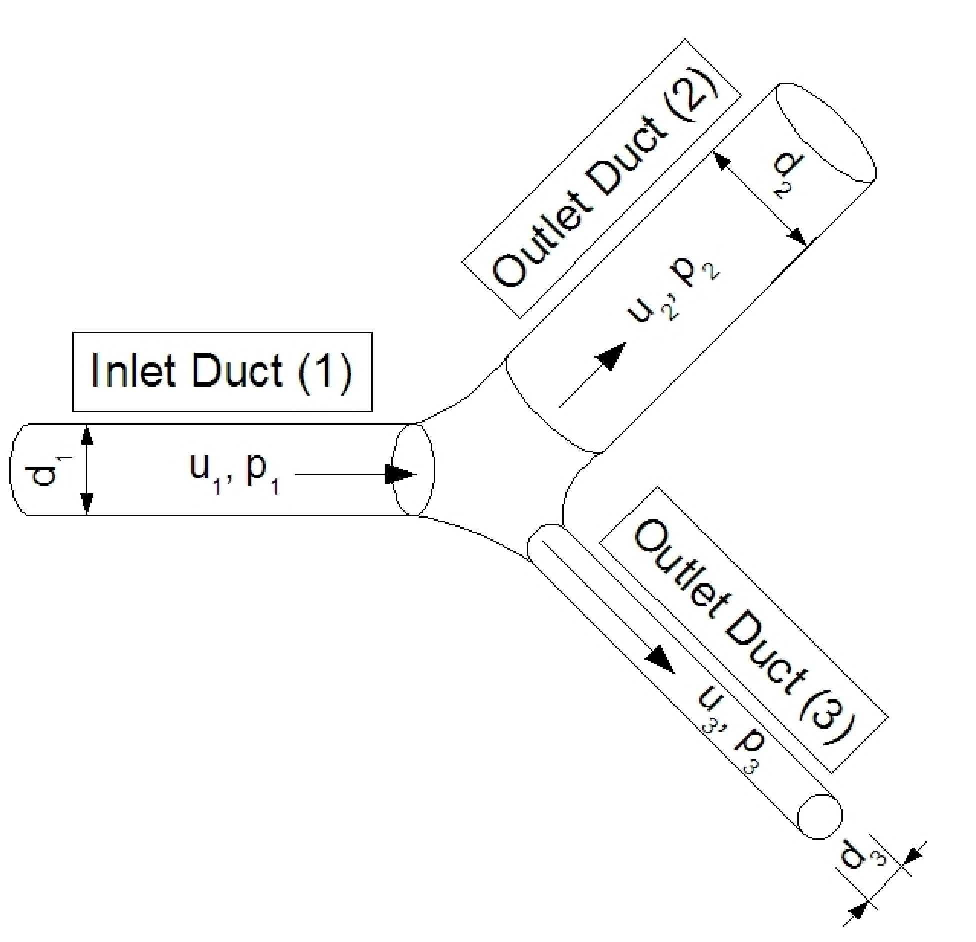
Collaborative Effort with Dimitrios Papavassiliou and Henry Neeman from OU (began Fall 2004)

Simulation of Flow of Fluids through Porous Media

Code FTPM – Flow Through Porous Media.

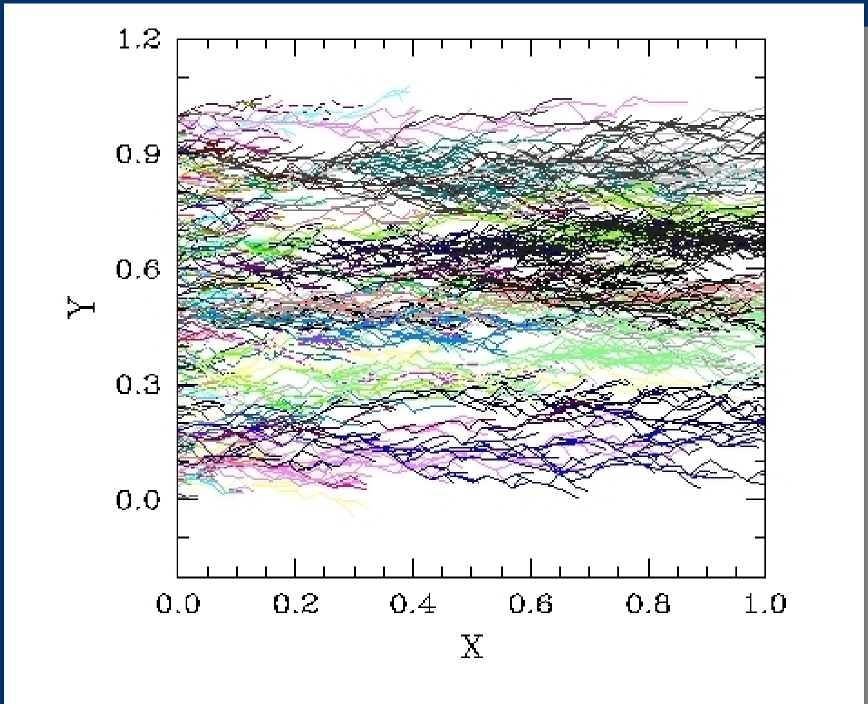
Solves for velocity and pressure at pore junctions in a randomly generated pore network.

Flow Network Analysis



Design and Analysis of networks depends on knowledge of flow and energy losses in arbitrary branches. No systematic studies to generalize these bifurcations

Porous Network Simulator (Collaboration with Univ. of Oklahoma)

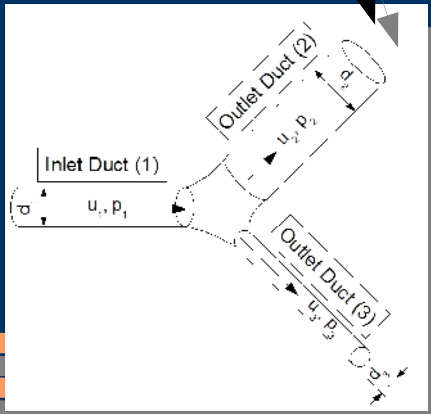


3D Monte Carlo networks from normal, beta, or empirical distribution (pore size pdf)

Coordination Number (1, 2, 3)

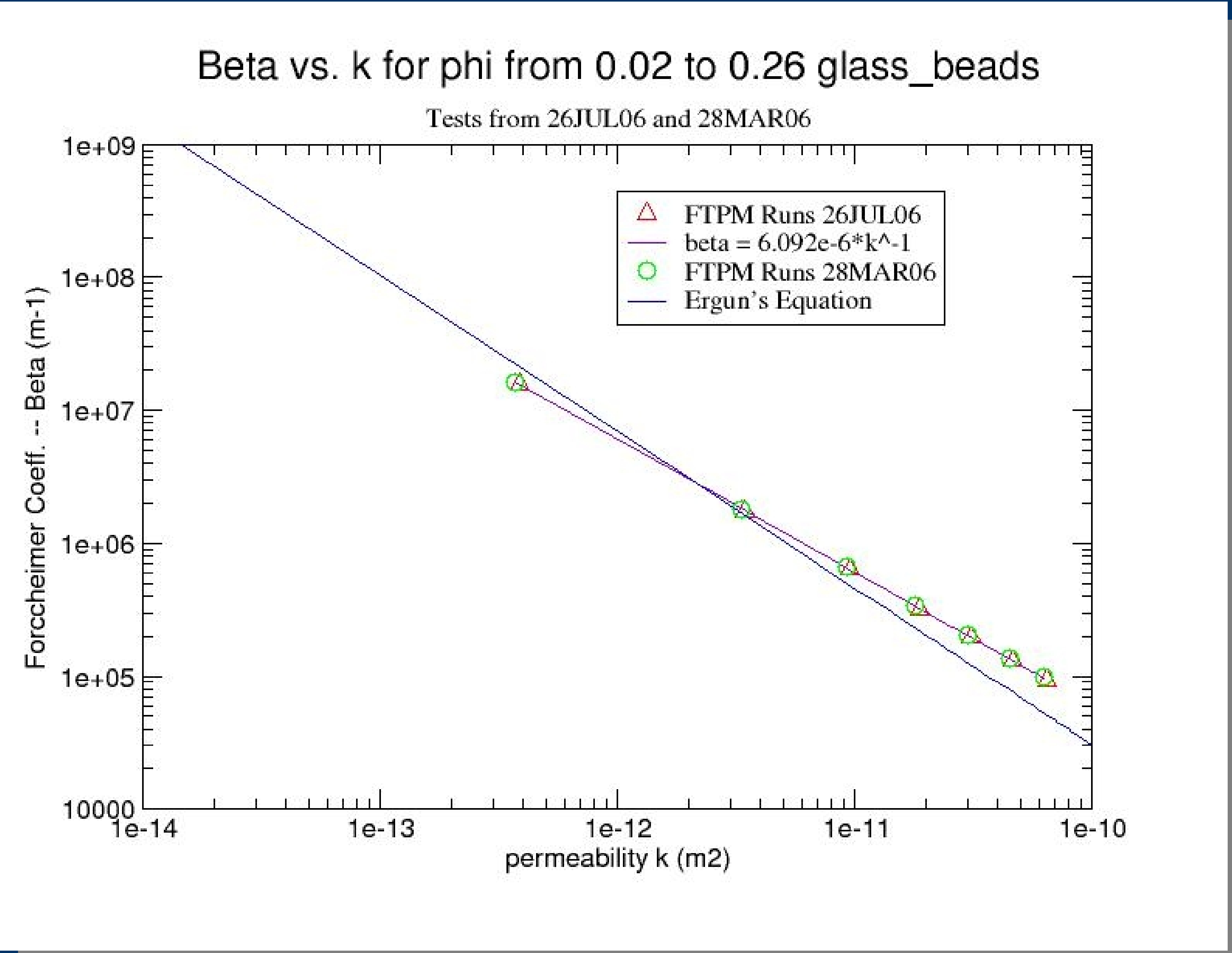
number of pores entering and leaving a junction

$\theta \pm 90^\circ$

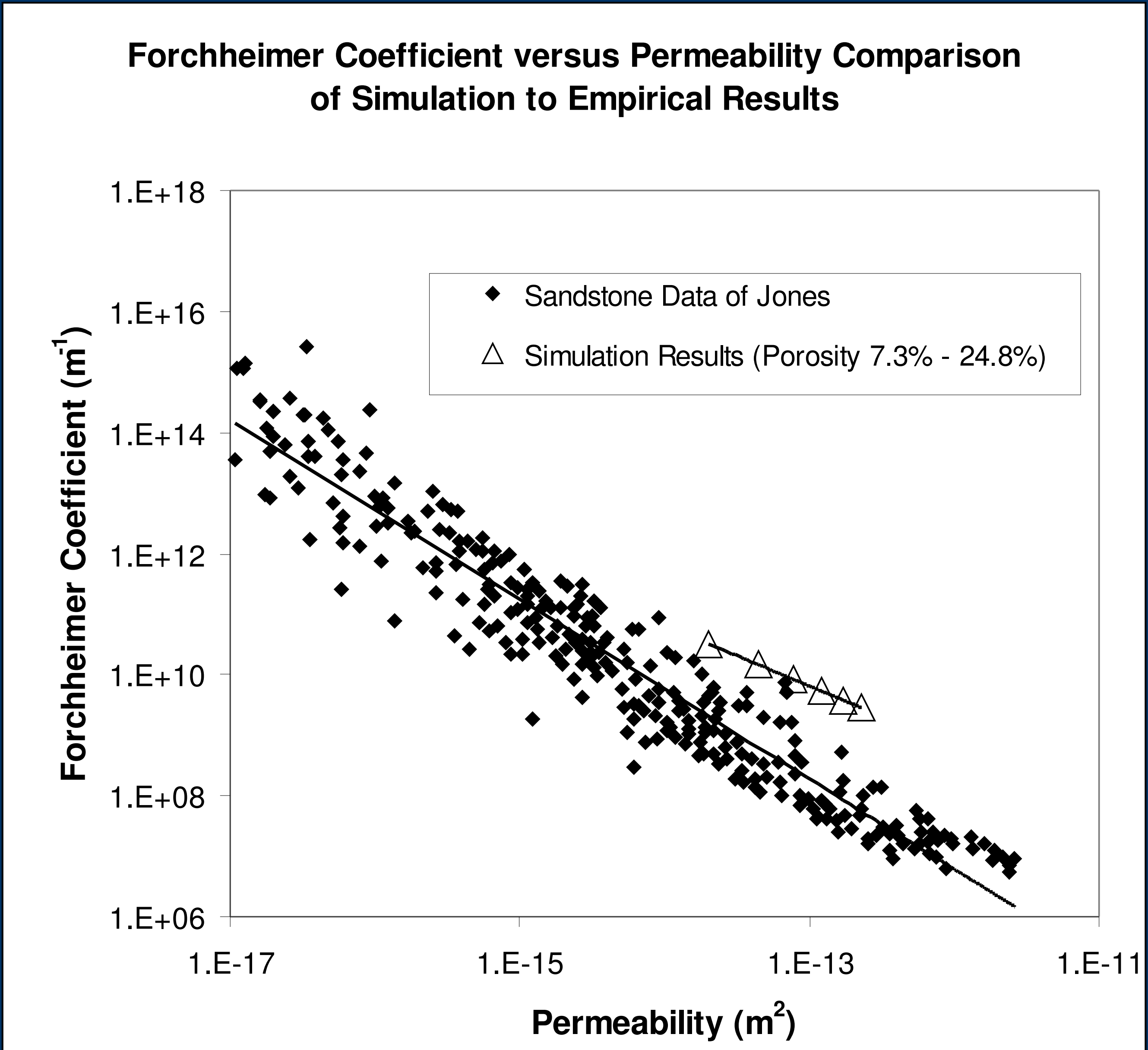


Projection on the xy plane of a 3D network that has 200 entry points at x=0, porosity equal to 10% and a range of ±60˚ relative to the x axis and ±30˚ relative to the y axis.

FTPM Results



FTPM Results



Literature

T's and Y's – limited configurations and most are for turbulent flow

Basset, M.D., Winterbone, D.E., and Pearson, R.J., 2001, "Calculation of Steady Flow Pressure Loss Coefficients for Pipe Junctions," Proc. Instn. Mech. Engrs., Part C, Journal of Mechanical Engineering Science, **215** (8), pp. 861-881.

W.H. Hager, 1984, "An Approximate Treatment of Flow in Branches and Bends," Proc. Instn. Mech. Engrs., Part C, Journal of Mechanical Engineering Science, **198**(4) pp. 63-9.

Blaisdell, F.W., and Manson, P.W., 1967, "Energy loss at pipe junctions," J. Irrig. and Drainage Div., ASCE, **93**(IR3), pp. 59-78.

Schohl, G.A., 2003, "Modeling of Tees and Manifolds in Networks," *Proceedings of the 4th ASME/JSME Joint Fluids Engineering Conference*, **2**, Part D, pp. 2779-2786.

Bassett, M.D., Pearson, R.J., and Winterbone, D.E., 1998, "Estimation of Steady Flow Loss Cofficients for Pulse Converter Junctions in Exhaust Manifolds," *IMechE Sixth International Conference on Turbocharging and Air Management Systems*, IMechE HQ, London, UK, **C554**/**002**, pp.209-218.

Ruus, E., 1970, "Head Losses in Wyes and Manifolds," J. Hyd. Div., ASCE, **96**(HY3), 593-608.

Laminar loss coefficients and elbows, reductions, contractions – much *larger loss coefficients than turbulent case – strong dependence on Reynold's number*.

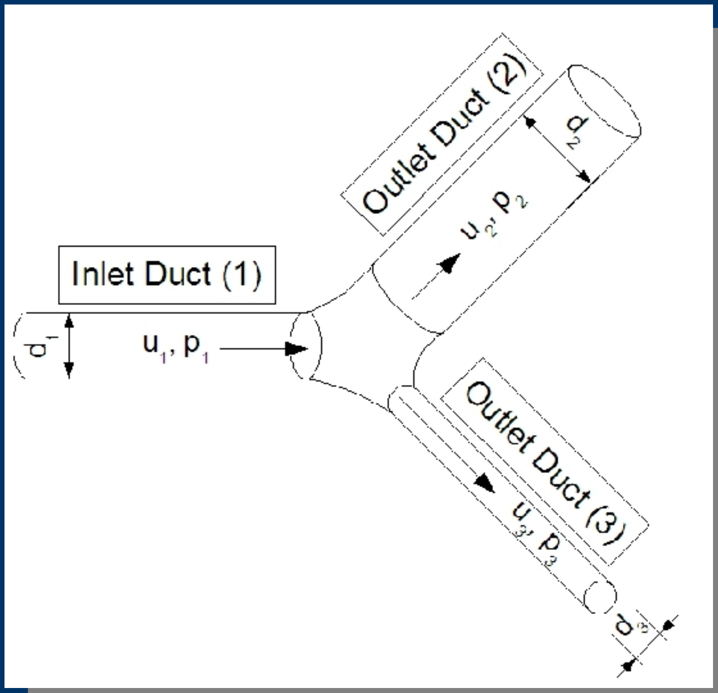
Edwards, M.F., Jadallah, M.S.M., and Smith, R., 1985, "Head Losses in Pipe Fittings at Low Reynolds Numbers," Chem. Engr. Res. Des., **63**(1), pp. 43-50.

Importance of roughness at microscale

Problem Description

Stagnation Loss Coefficient

$$K_2 = \frac{\left[\left(\frac{p_1}{\rho} + \frac{u_1^{\,2}}{2}\right) - \left(\frac{p_2}{\rho} + \frac{u_2^{\,2}}{2}\right)\right]}{\frac{u_1^{\,2}}{2}}$$



Parameters:

d_2/d_1, d_3/d_1

θ_2 and θ_3

f_2 (this sets f_3) – (why? other literature and possibility of simulations where this is unknown initially)

Automation of Geometry Generation and CFD Runs

Custom Code was written to:

(a) create GAMBIT journal files that instantiate the desired geometry *based on existing 2D geometries.*

(c) create a script that loads journal files into GAMBIT and meshes

(d) create all necessary preprocessing files for FLUENT.

(e) create post-processing files for FLUENT results and to tabulate results for a complete set of runs

Solution Methodology
2D Geometry Generalization

$L_1 = 5\ d_{max}$

L_2 and $L_3 = 10d_{max}$

If $d_2 > d_{avg}$,

then $r_2 = 3d_2$;

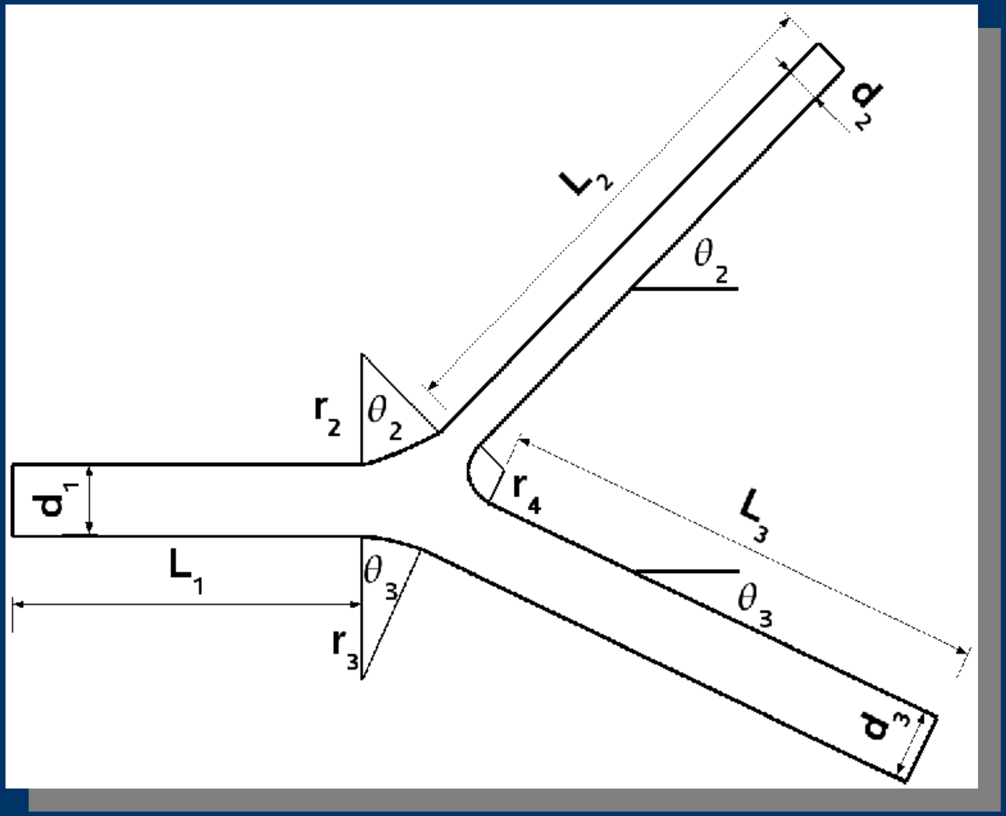
else $r_2 = 2d_2$

If $d_3 > d_{avg}$,

then $r_3 = 3d_3$;

else $r_3 = 2d_3$

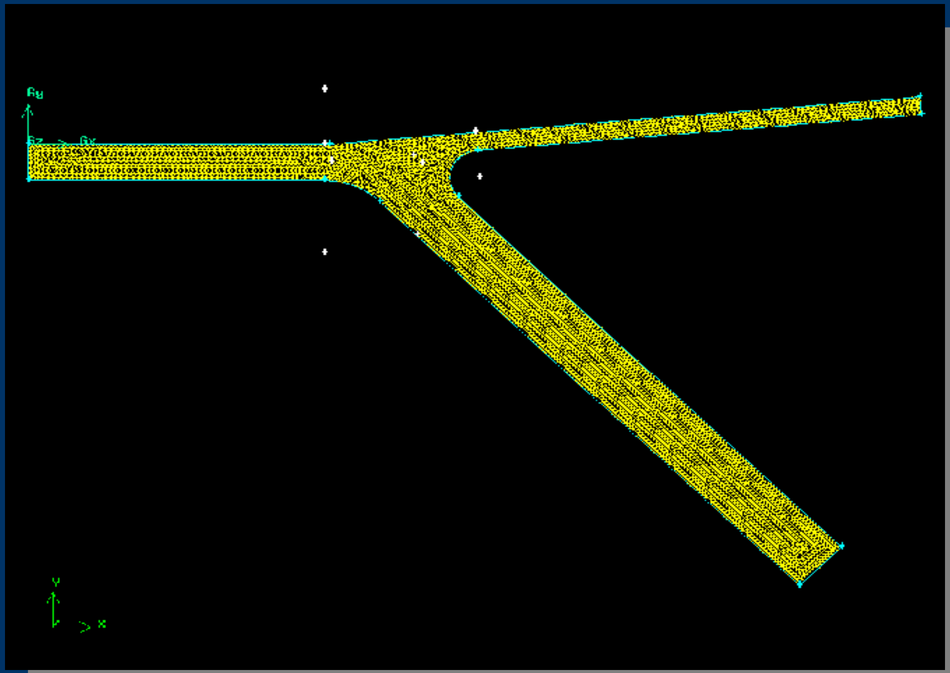
$r_4 = d_{max}/2$

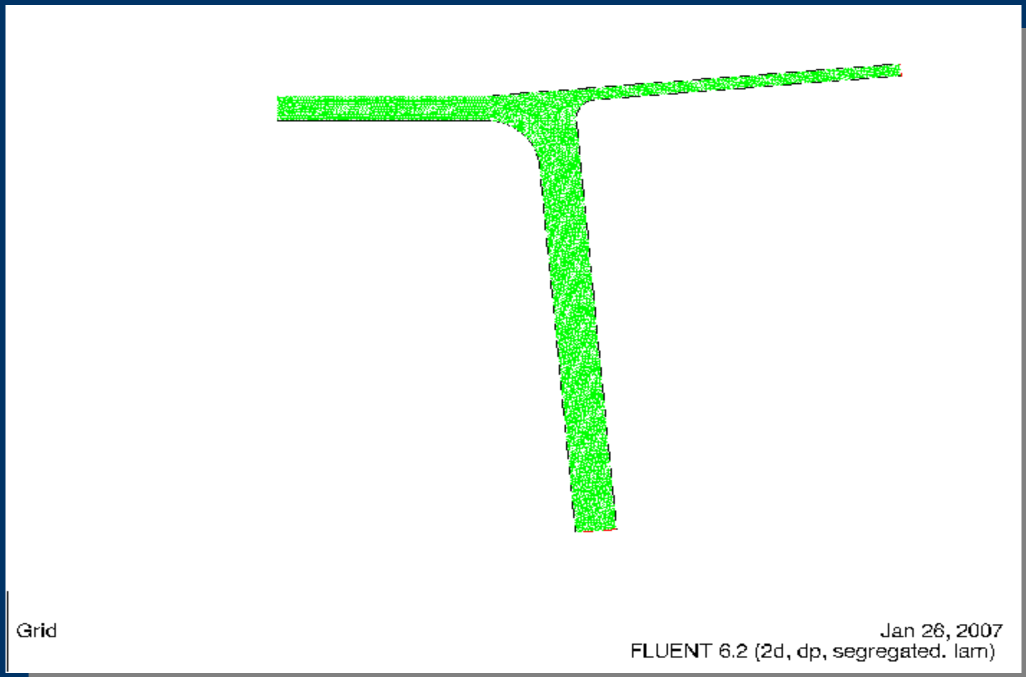


Generalized Geometry

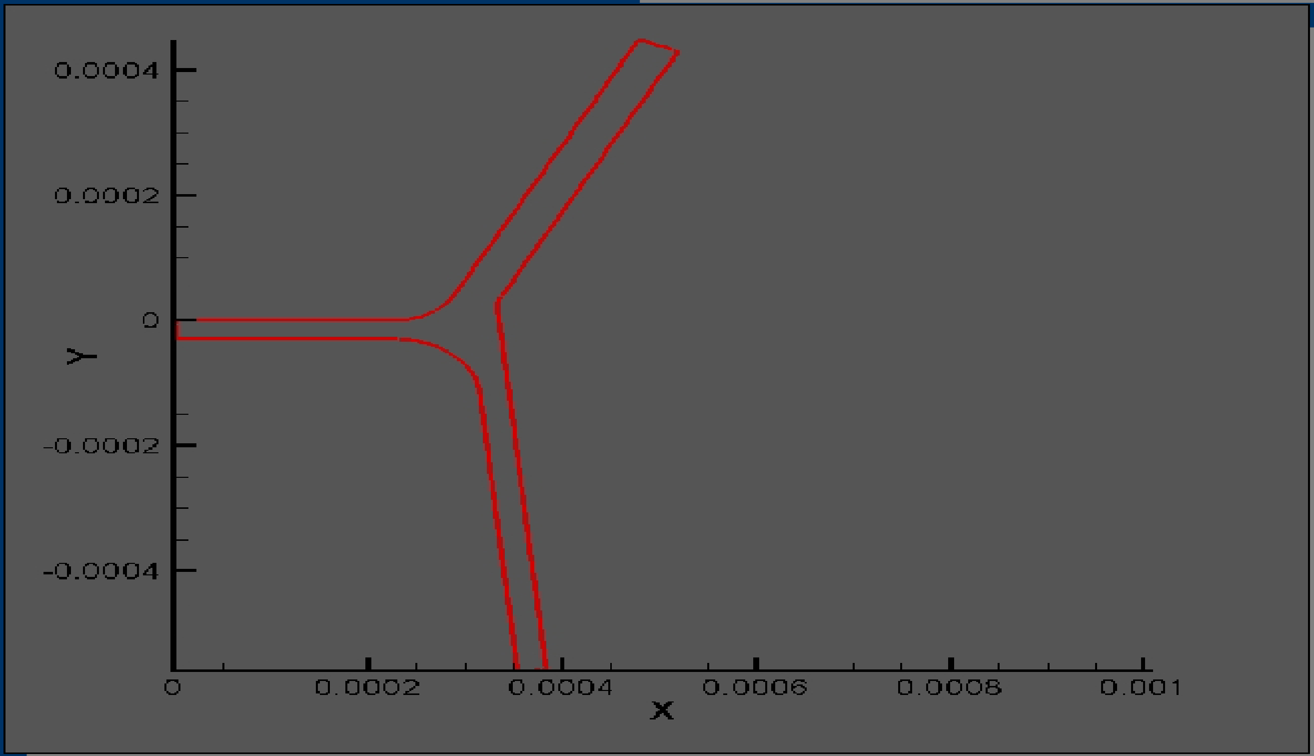
larger and smaller outlet ducts ; 2Dim. - 3Dim are underway

avoid sharp edges ; 5 – 90 degrees for angles



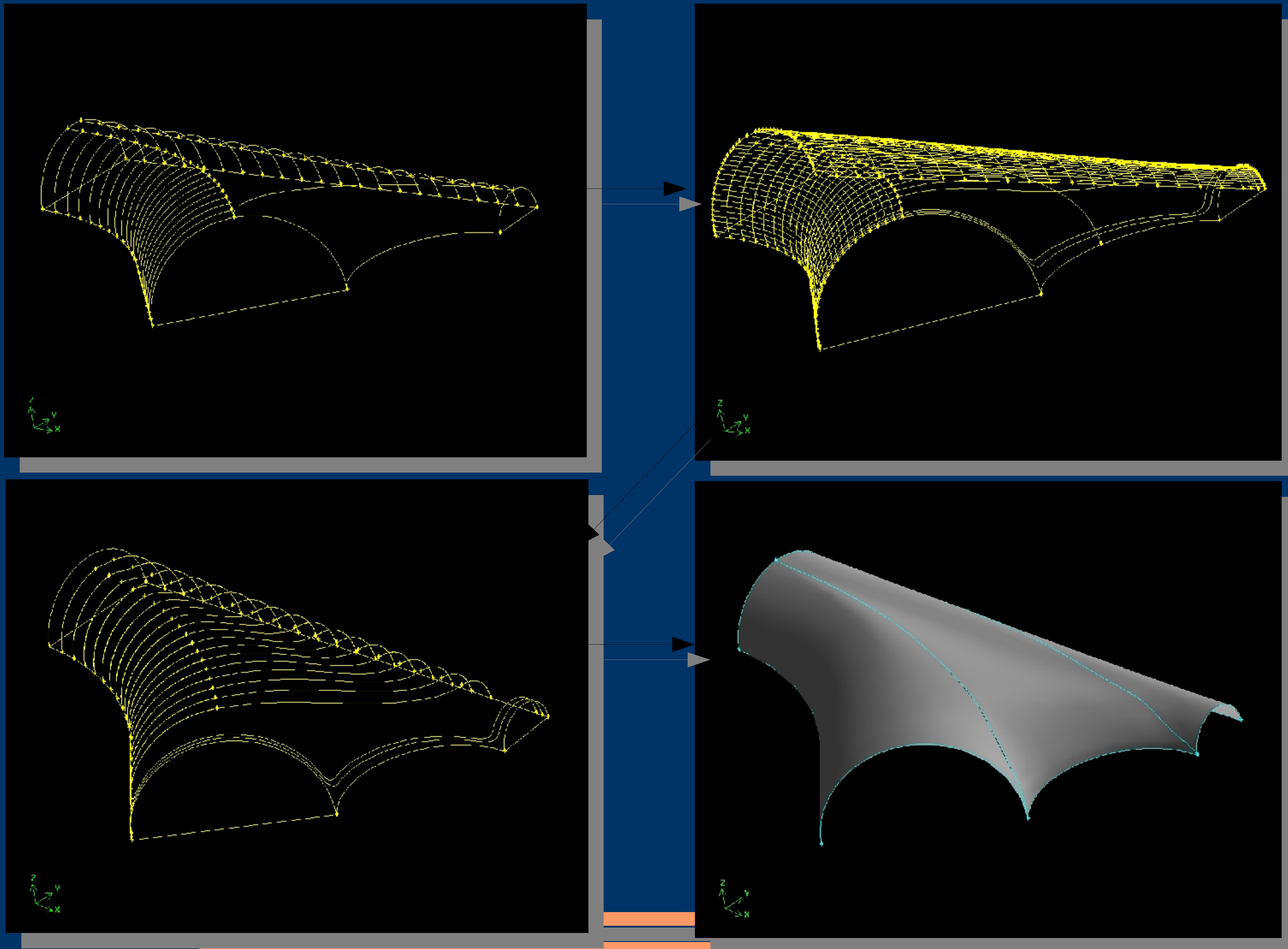


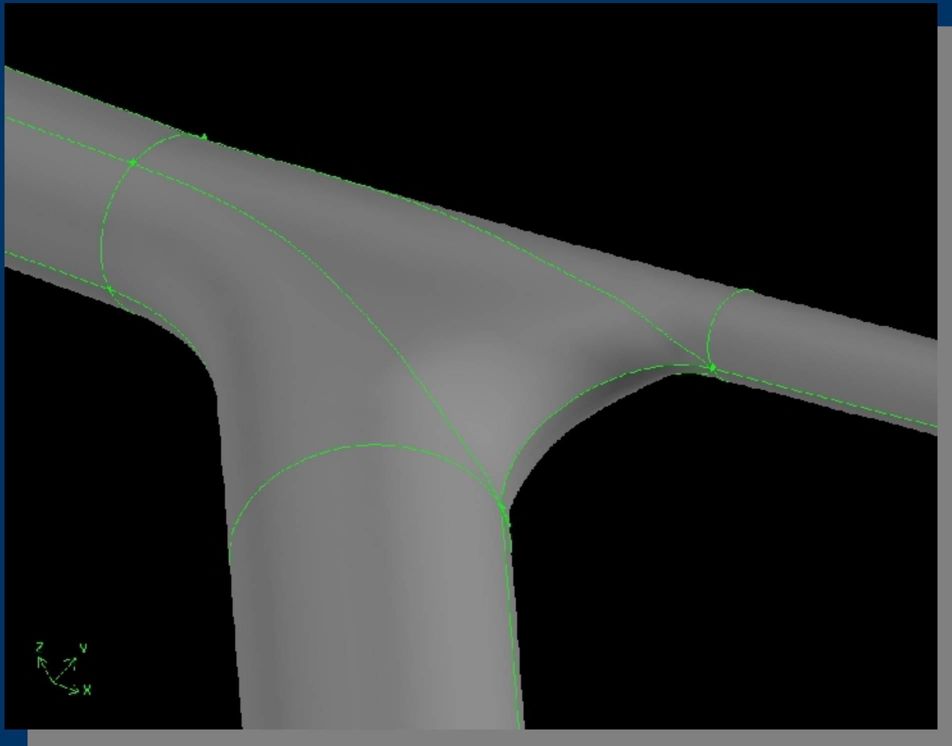
Grid
Jan 26, 2007
FLUENT 6.2 (2d, dp, segregated. lam)

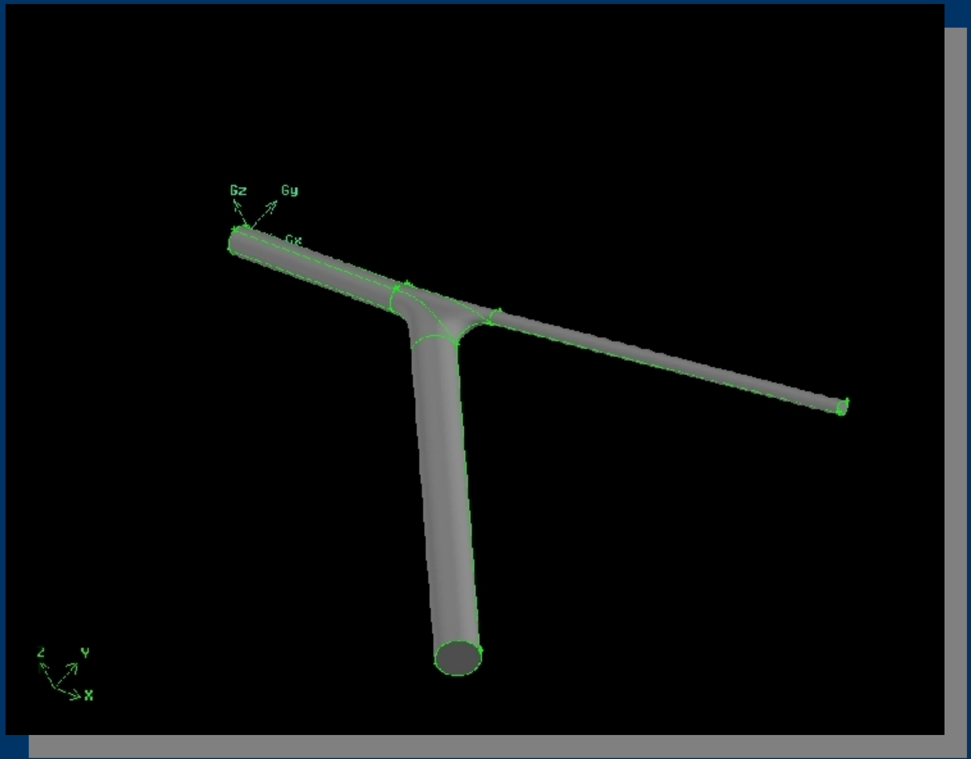


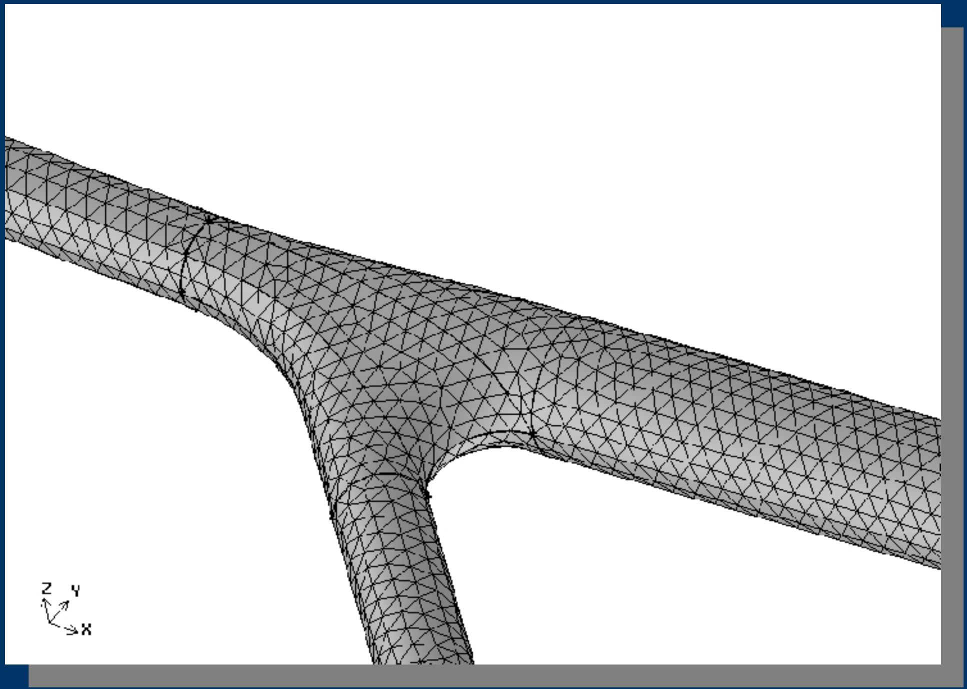
0.0004
0.0002
0
-0.0002
-0.0004
Y
0
0.0002
0.0004
0.0006
0.0008
0.001
X

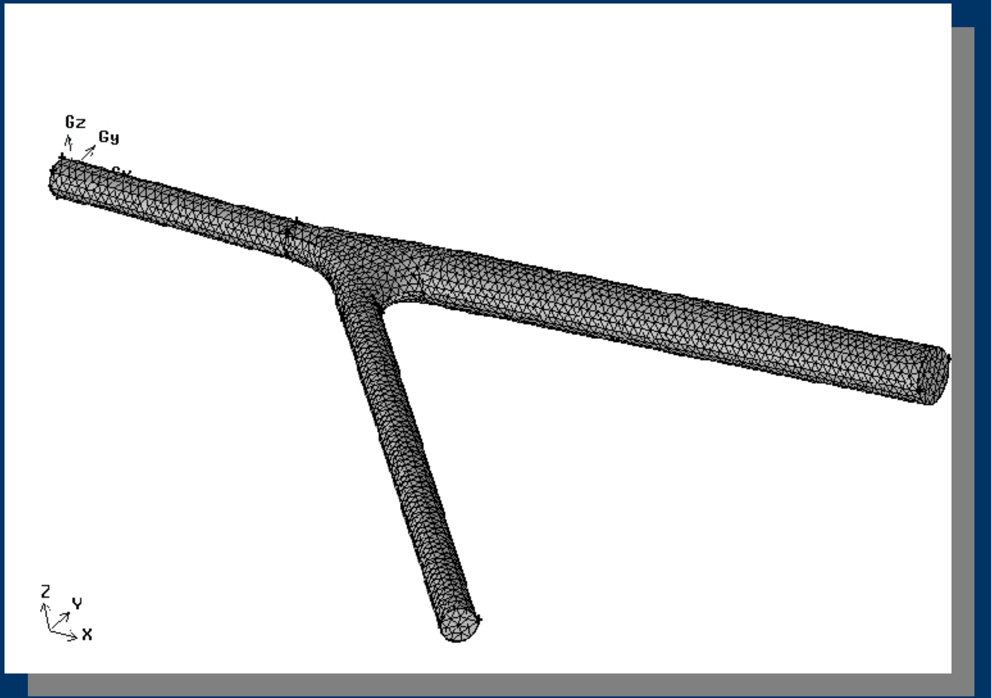
3D Geometry – Mark I




Z Y X


Gz Gy
Z Y X


Z Y X


Gz Gy
Z Y X

Simulation Parameters

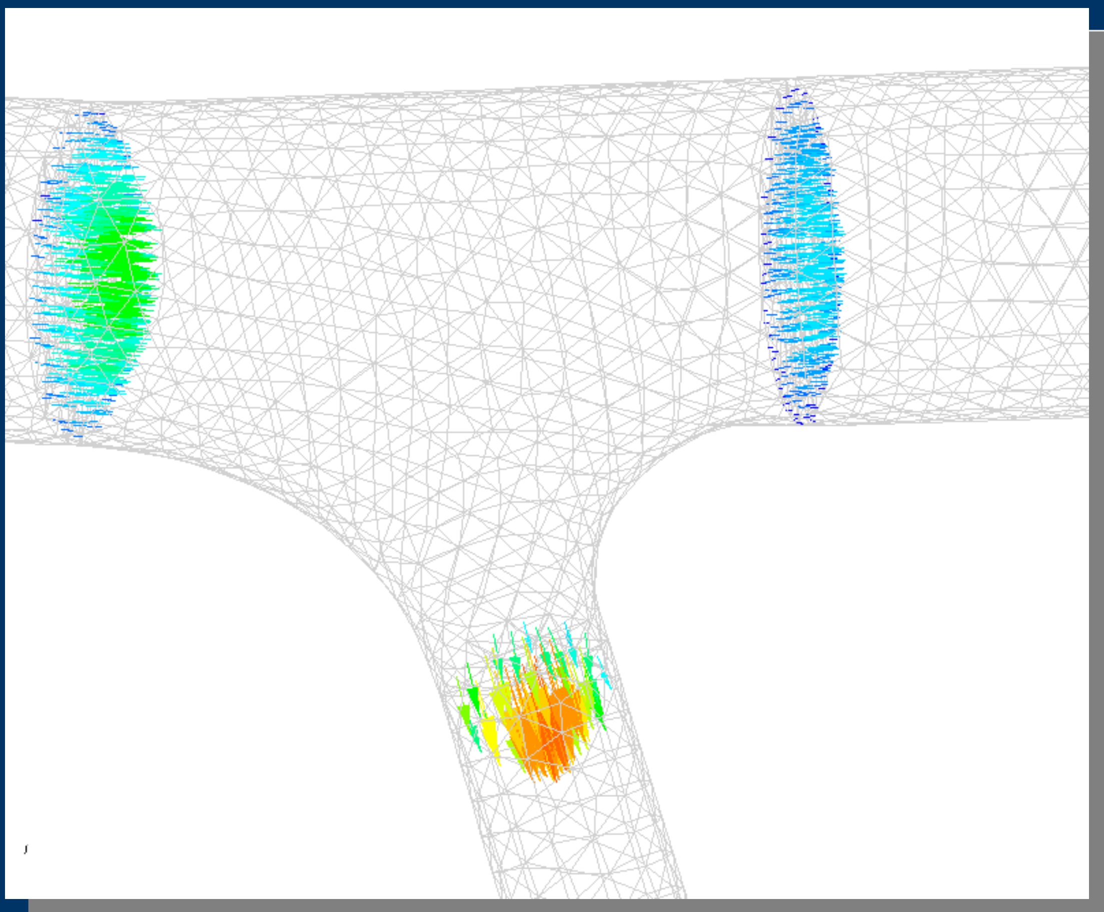
Re_D was maintained at constant value at the inlet duct

d_1 was 30 microns. The fluid was chosen to be liquid water at 20˚C. The inlet flow velocity, u_1, was set to 0.5 m/s giving a Reynolds number of 15

$Le_D = 0.06Re_D$ D --- gives 0.9 D for $Re_D = 15$

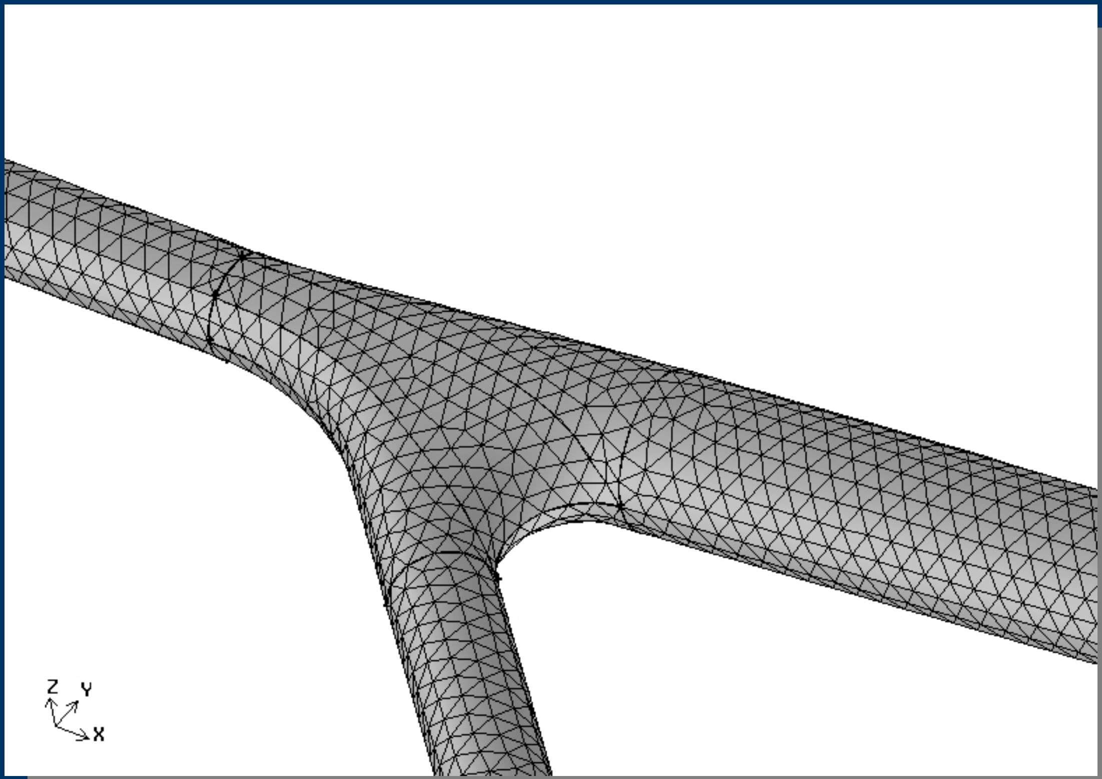
FLUENT output files contain surface averaged static pressure and magnitude of flow velocity at duct cross-sections at the duct inlets and exits.

Duct Inlet/Outlets



Duct inlet and exit sections considered to be where geometry of duct is the same as the downstream portion for outlets and upstream portion for inlet.

Mesh Automation



- Mesh was set to 1/4 of smallest duct
- Tetrahedral Mesh
- Large number of tests to assess ability to generalize the mesh (1/4 factor determined in this manner)
- Some testing to verify no change in results with change in mesh size.
- Inlet was specified as velocity inlet
- Outlets were outflow boundaries – allowed specification of flow fraction

Numerical Methods

Finite Volume solution of integral Navier Stokes
Steady-State 3D
Implicit
SIMPLE for pressure velocity coupling
1st order upwind scheme of momentum discretization
Max number of iterations
Convergence criterion = 0.1%

Parameter Values

d_2/d_1 and d_3/d_1 = 0.5, 1.0, 1.5

f_2 = 0.1, 0.3, 0.5, 0.7, 0.9

灼$_2$ and 灼$_3$ = 5˚, 25˚, 45˚, 65˚, 85˚

600 runs attempted – 475 completed (*geometry issues on remainder*)

Suite of C++ procedures to create geometries, input files, read and collate results

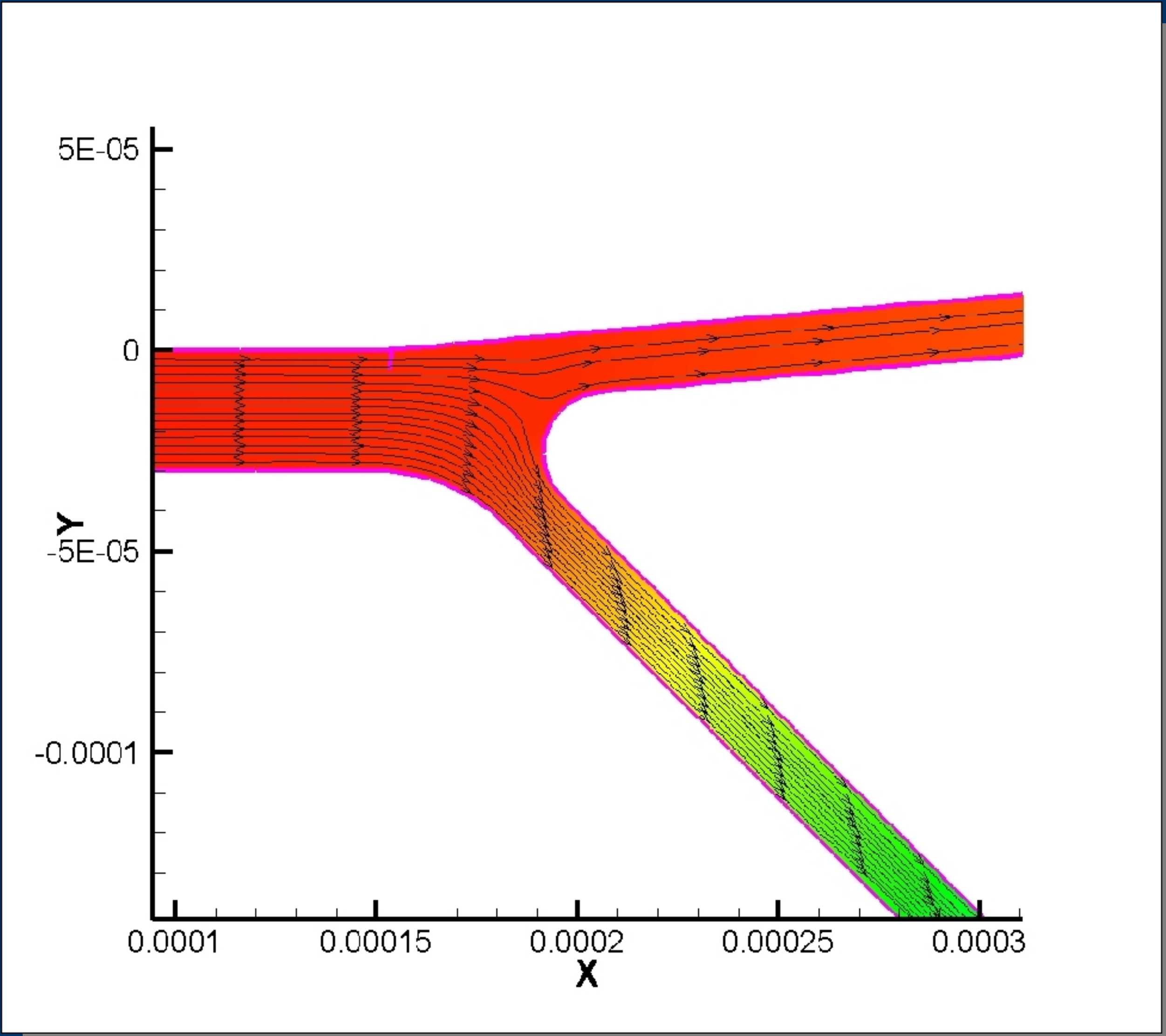
Create GAMBIT script to create geometries

Create input files for GAMBIT and FLUENT

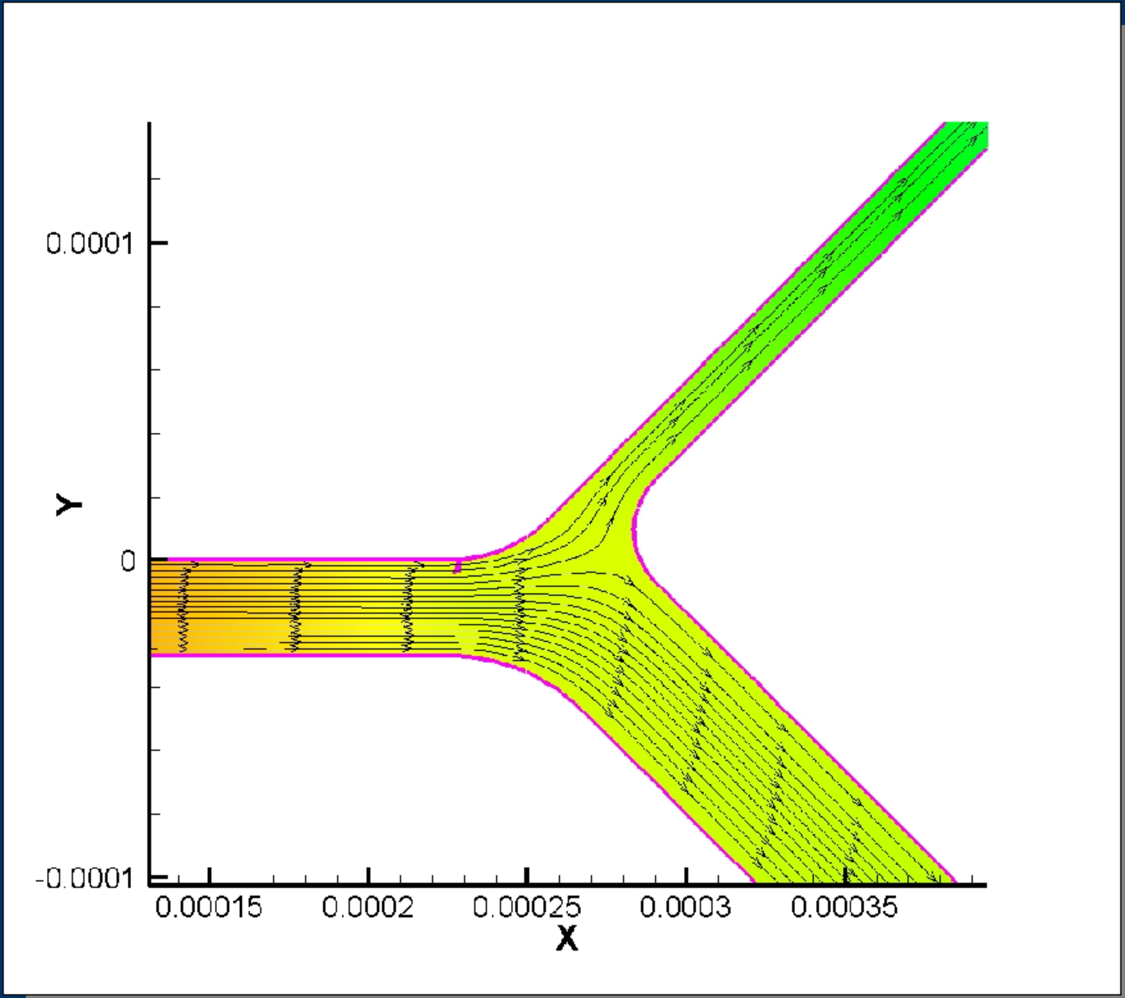
Read results files for static pressures and velocities averaged over surfaces in and out of junctions.

Fluent Result

f2 = 0.1, d2/d1 = 0.5, θ2 = 5˚, d3/d1 = 0.5, and θ3 = 45˚

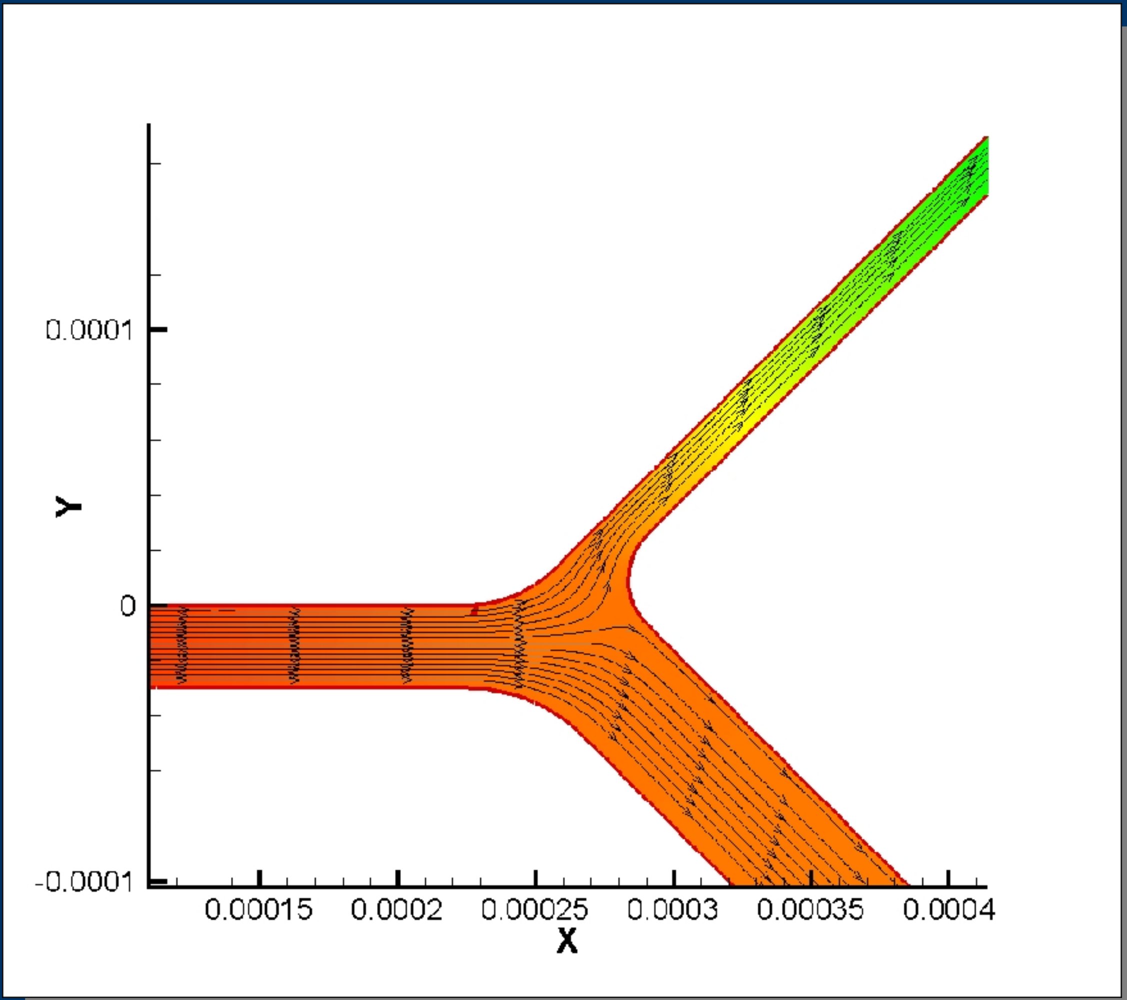


$f2 = 0.1$, $\theta 2=45°$, $\theta 3=45°$, $d2/d1=0.5$, $d3/d1=1.5$.



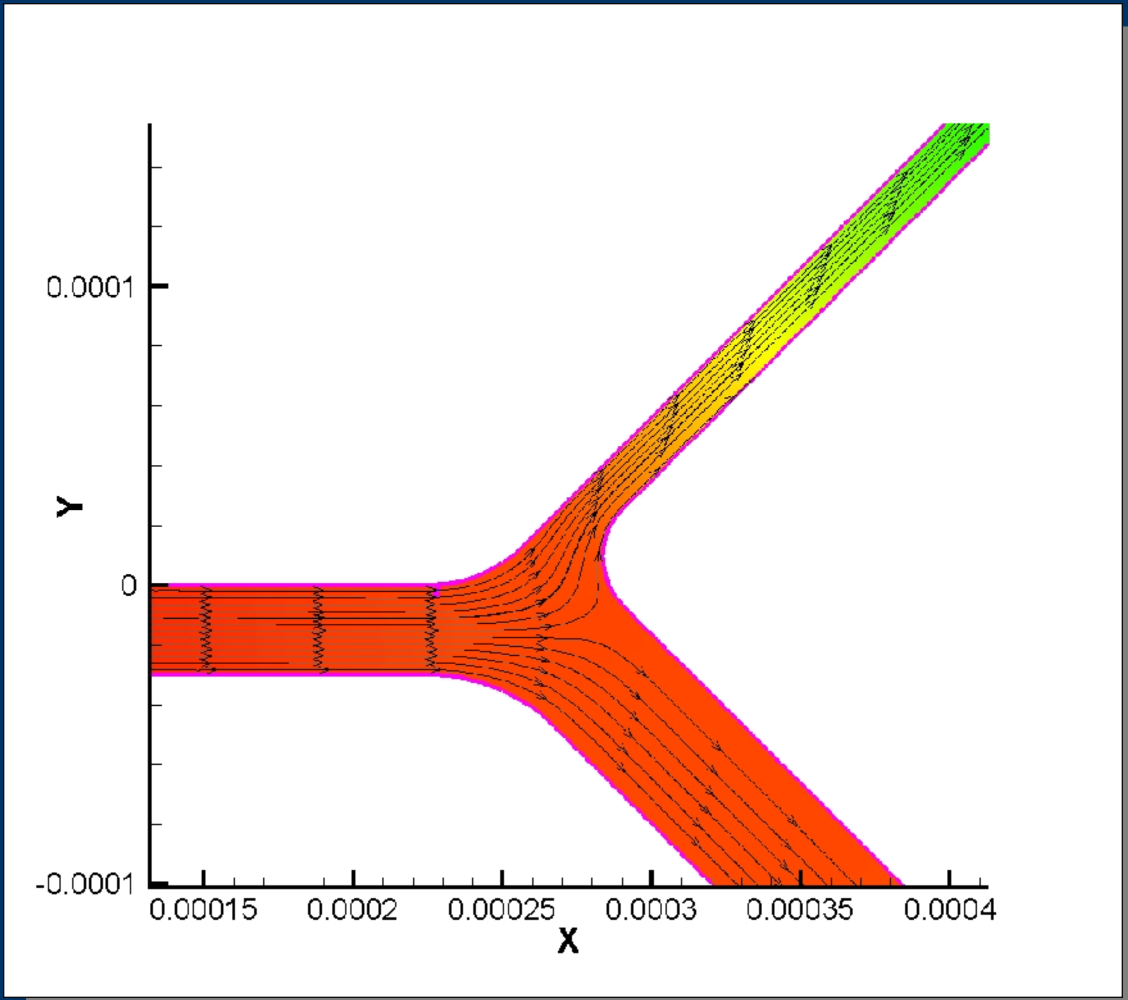
$K_2 = 5.47$

f2 = 0.3, θ2=65°, θ3=45°, d2/d1=0.5, d3/d1=1.5.



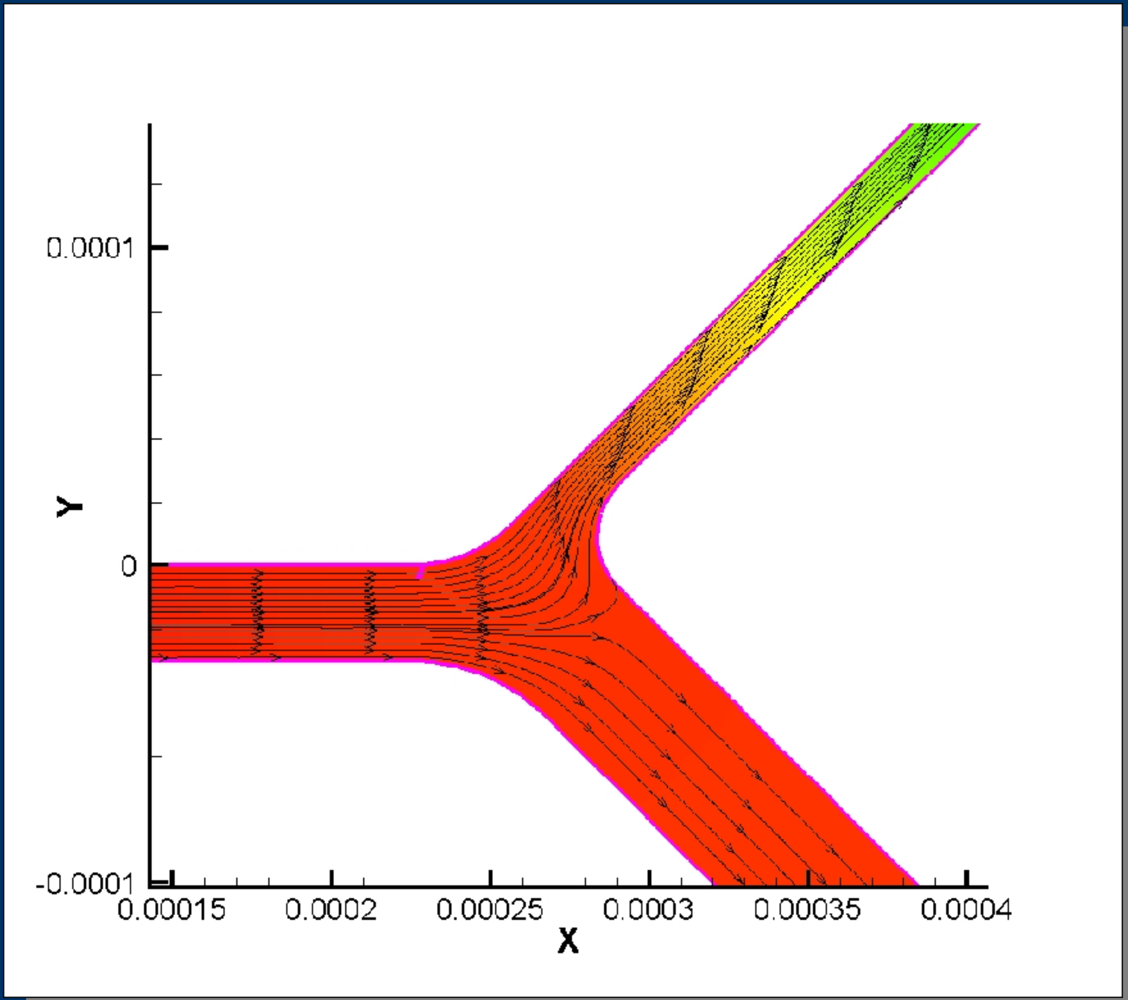
$K_2 = 11.6$

f2 = 0.5, θ2=65°, θ3=45°, d2/d1=0.5, d3/d1=1.5.



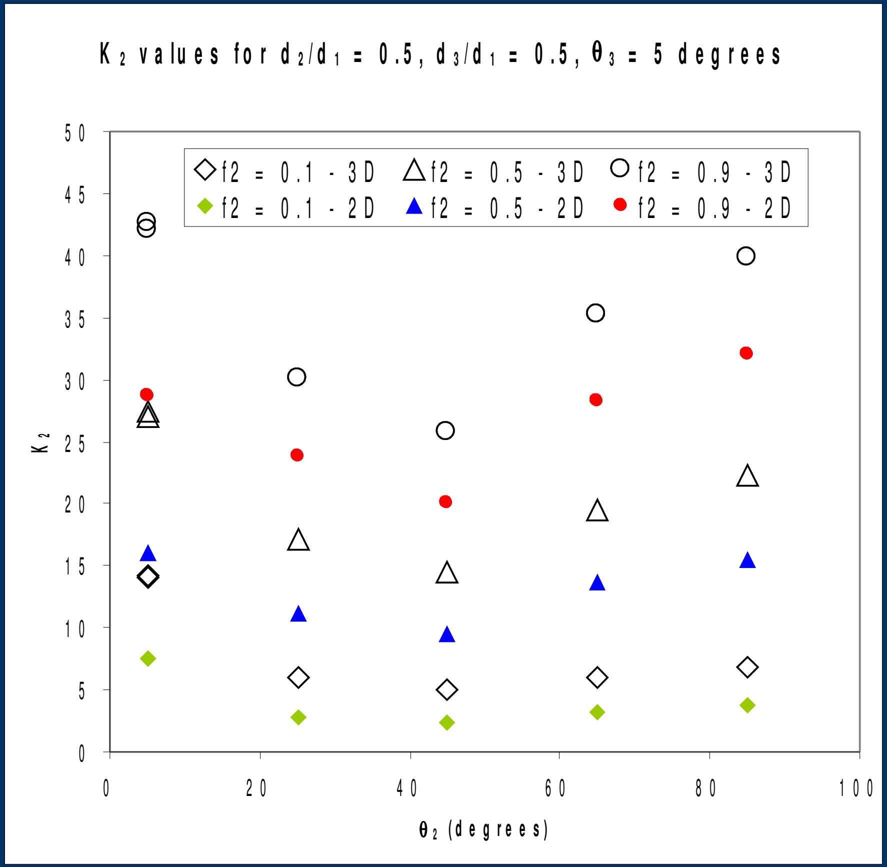
$K_2 = 18.4$

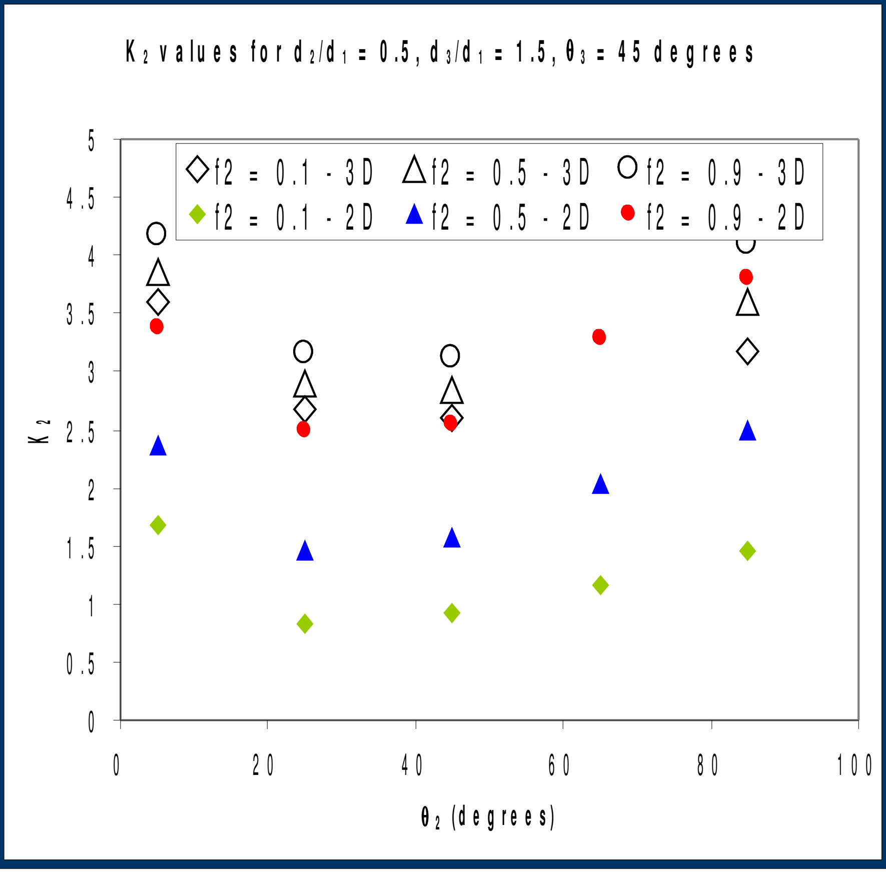
f2 = 0.7, θ2=65°, θ3=45°, d2/d1=0.5, d3/d1=1.5.



$K_2 = 25.7$

2D vs. 3D Differences





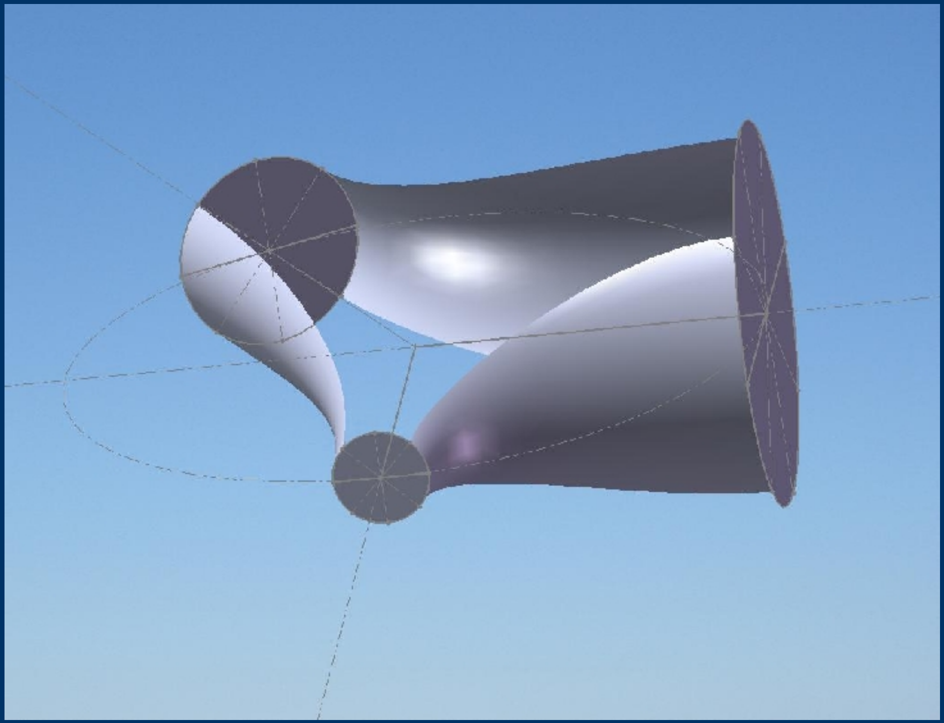
$$\left[\frac{k_2^{\,3D}}{k_2^{\,2D}}\right]_{average} = 1.55 \quad (std.\ \ dev.) = 0.45$$

$$k_2 = \frac{\Delta p/\rho}{u_1^{\,2}/2} - \frac{u_2^{\,2}}{u_1^{\,2}} + 1$$

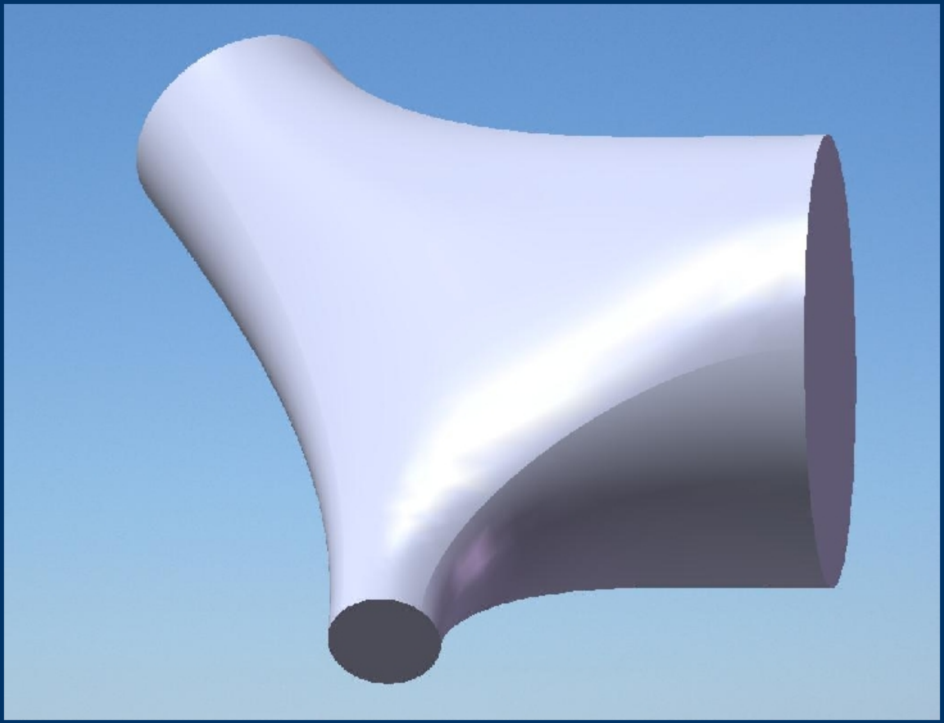
pressure effects

kinetic energy effects

3D Mark II Junction



Junction Without Surface Fills

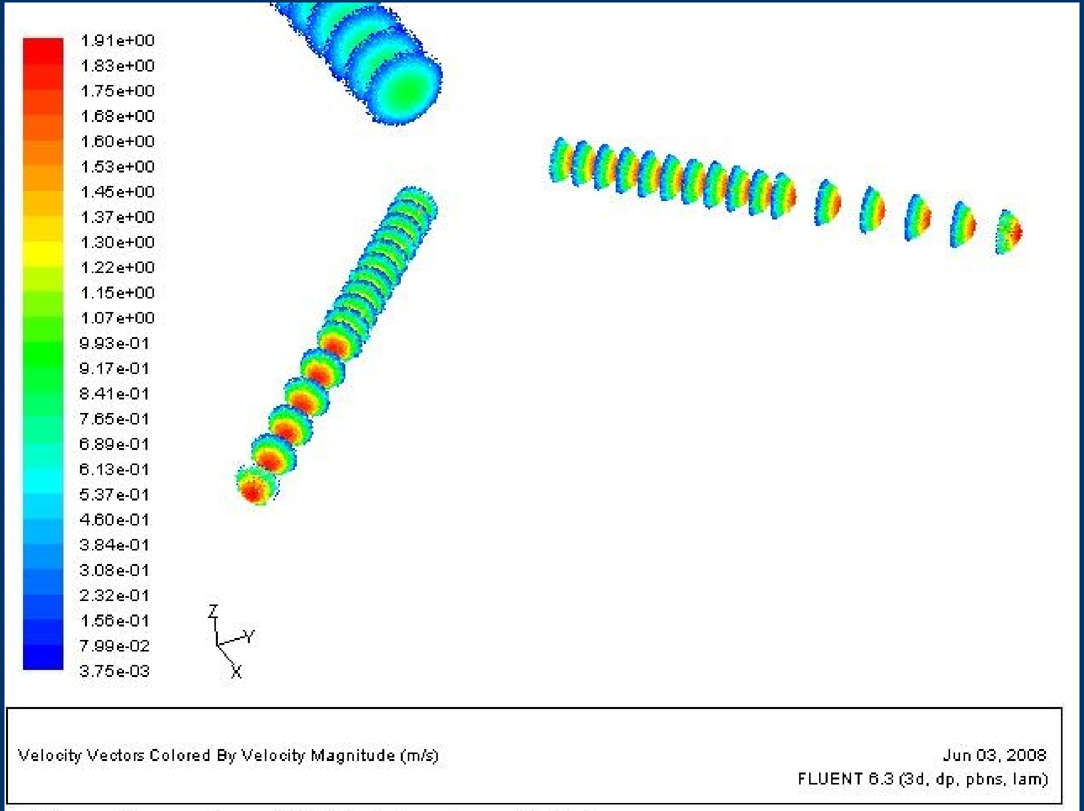


Junction With Surface Fills

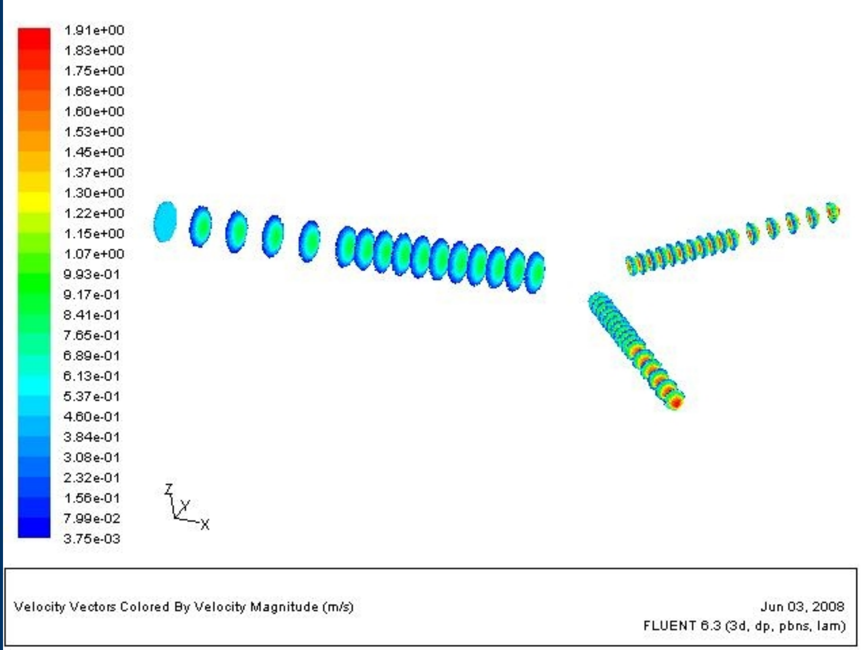
Initial Simulations – 3D Mark II

Small batch

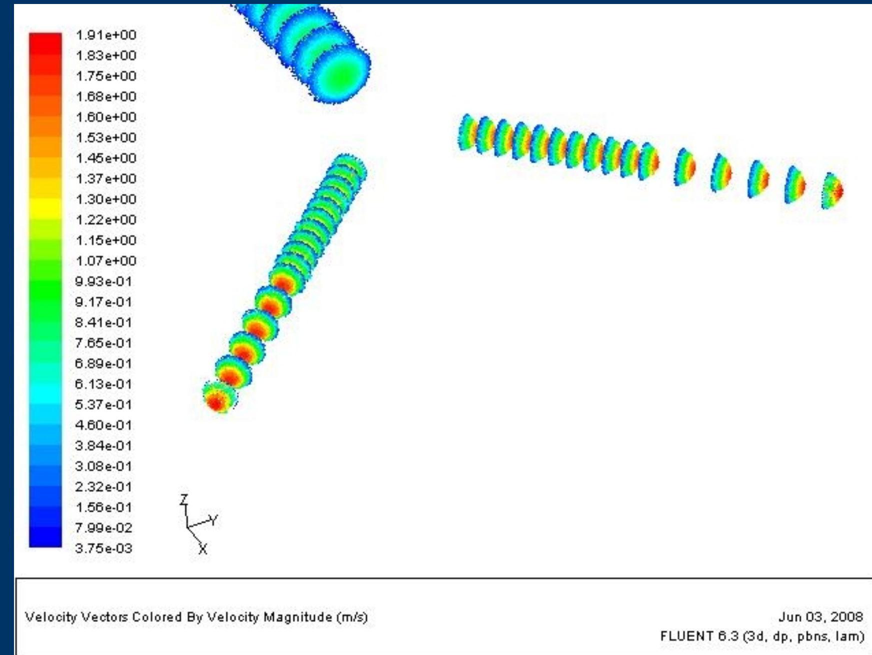
Comparable results to original 3D runs



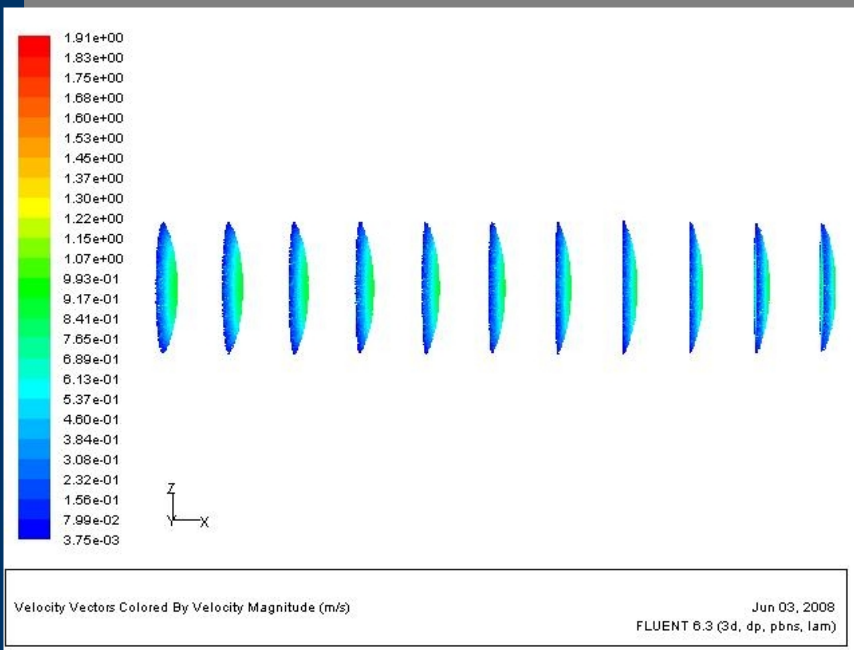
Reynolds number of 14 Inlet diameter of 30microns



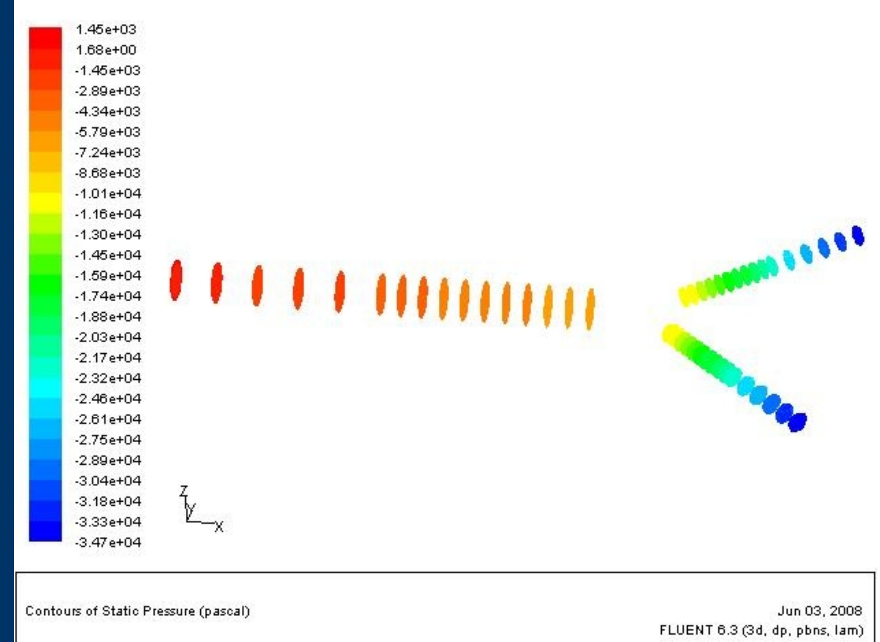
Reynolds number of 14 Inlet diameter of 30microns



Reynolds number of 14 Inlet diameter of 30microns



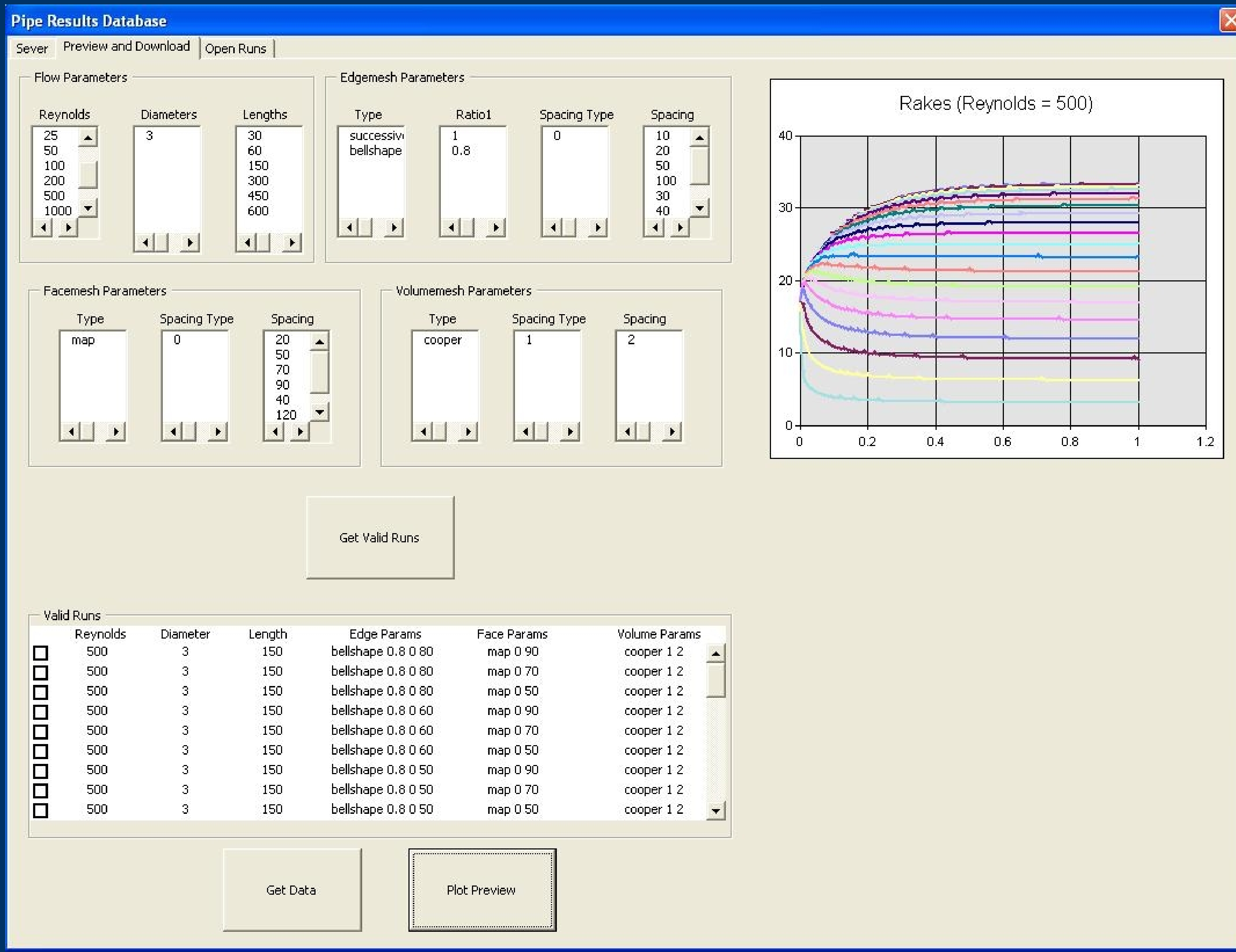
Reynolds number of 14 Inlet diameter of 30microns



Reynolds number of 14 Inlet diameter of 30microns

Pipe Mesh Testing

Database Interface



Pipe Mesh Testing

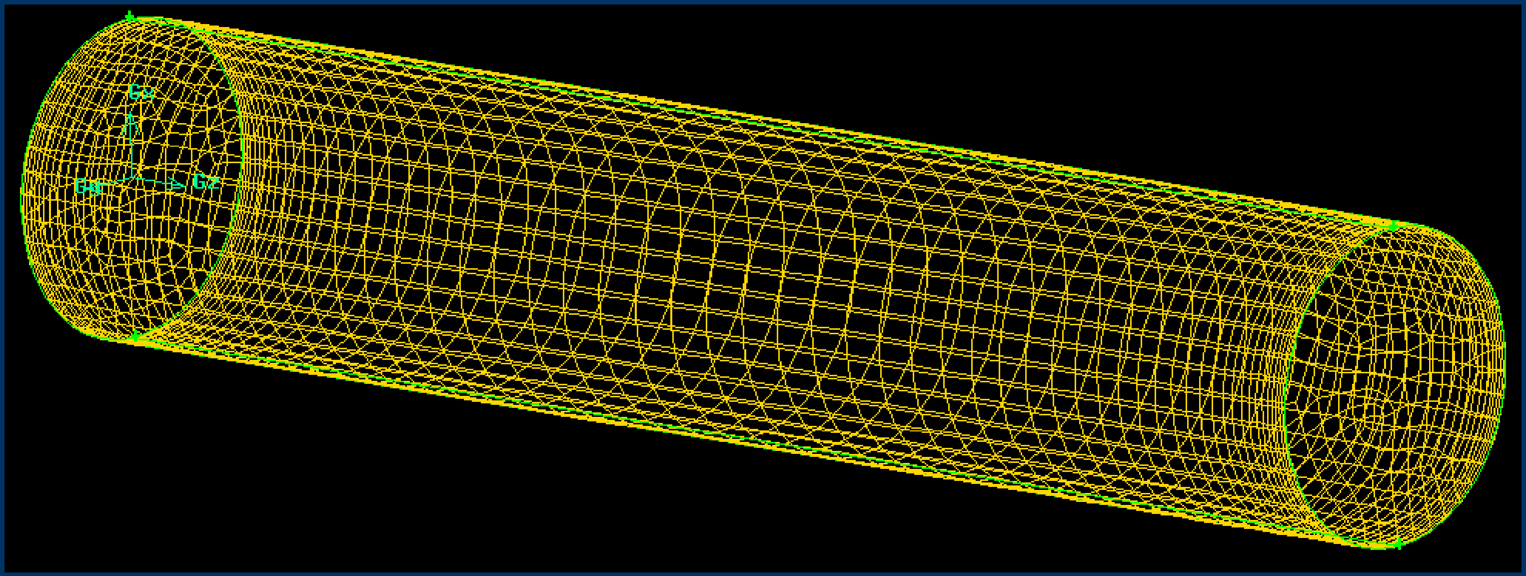
Flow-aligned hex core

Varied axial and radial spacing

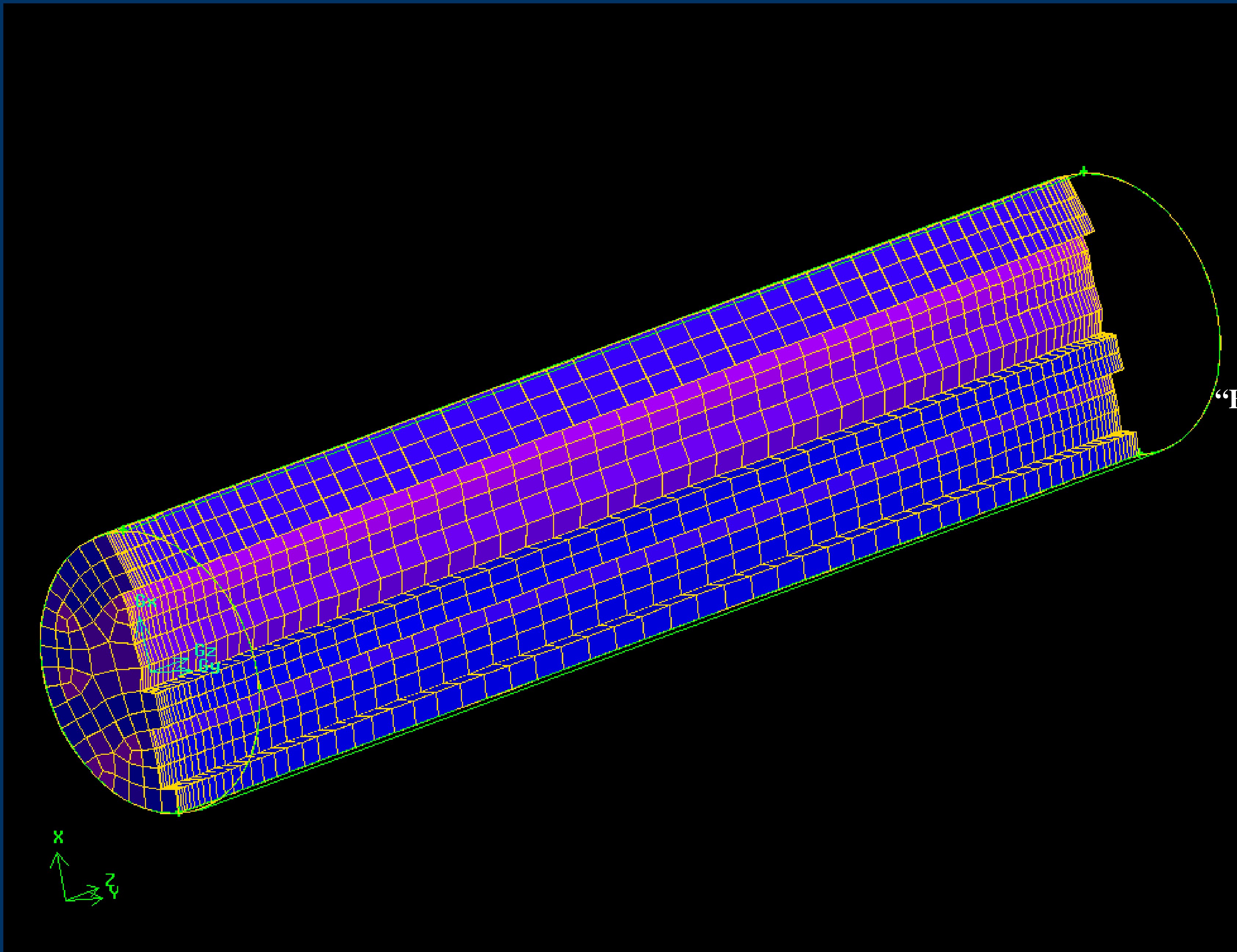
MySQL results database

Automated

Results database easy to setup for junction runs

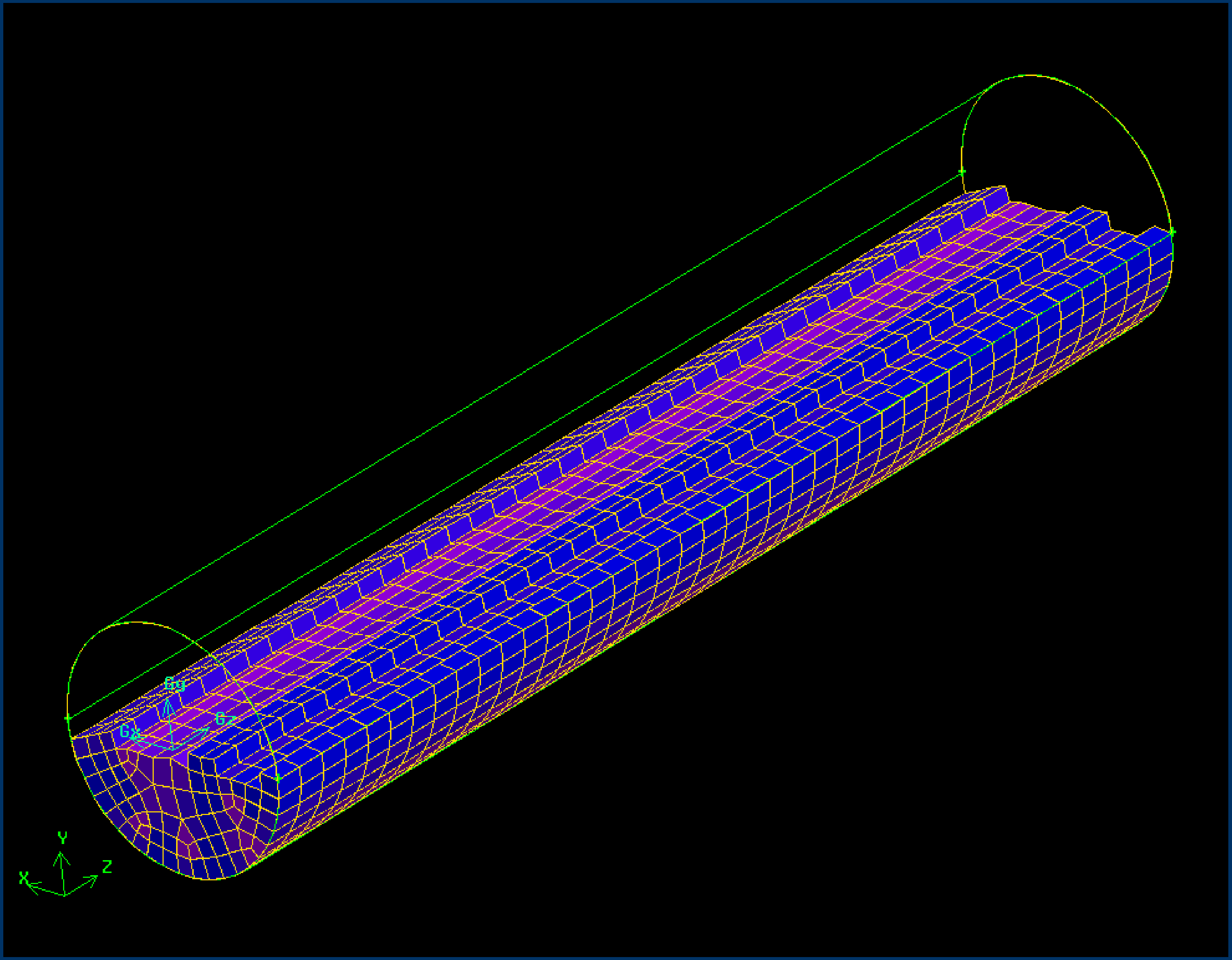


Pipe Mesh Testing



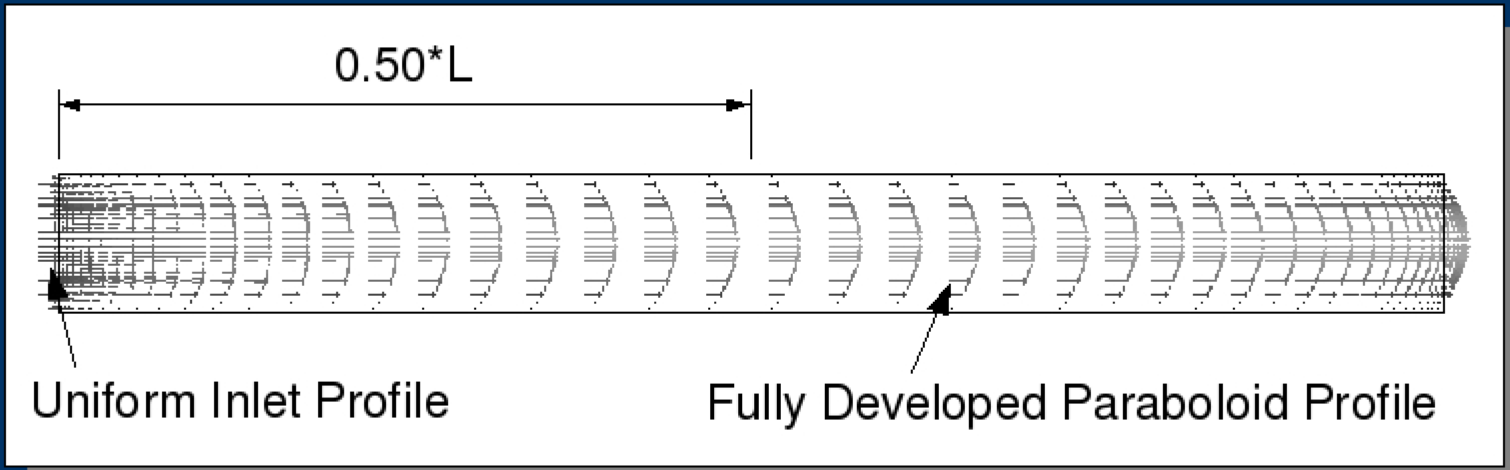
“Bell Shaped” Axial Spaci

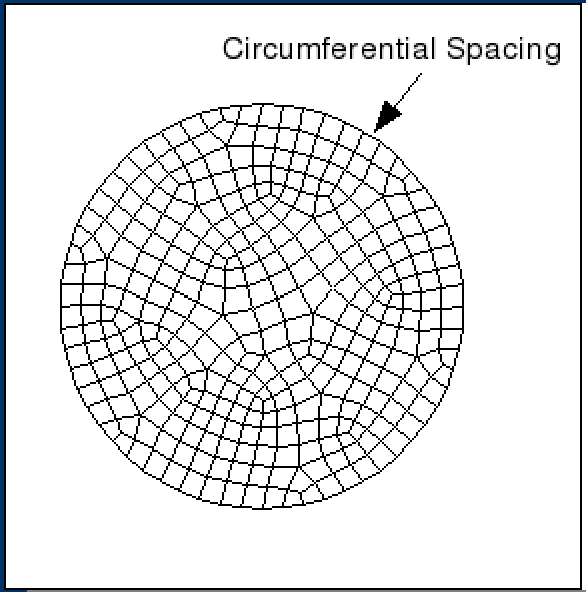
Pipe Mesh Testing

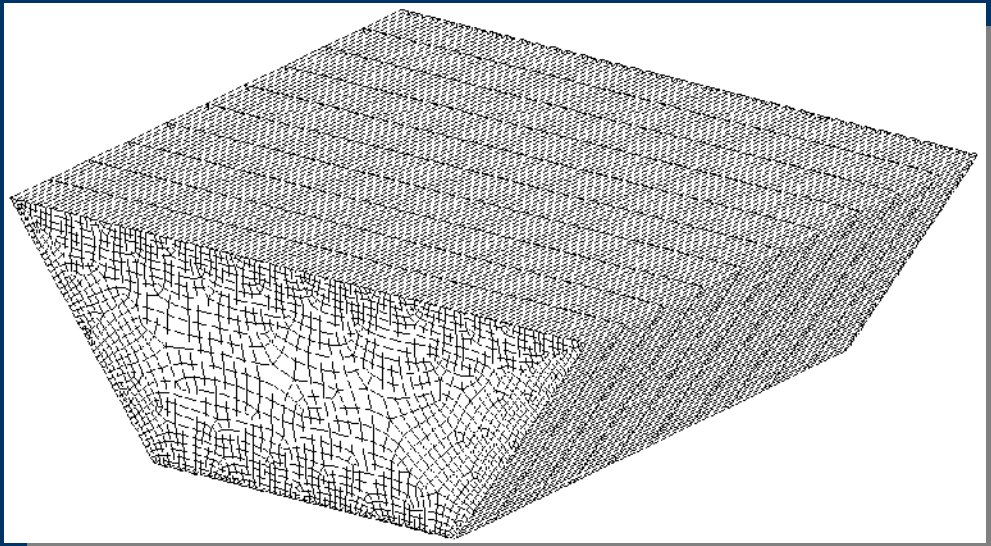


Uniform Axial Spacing

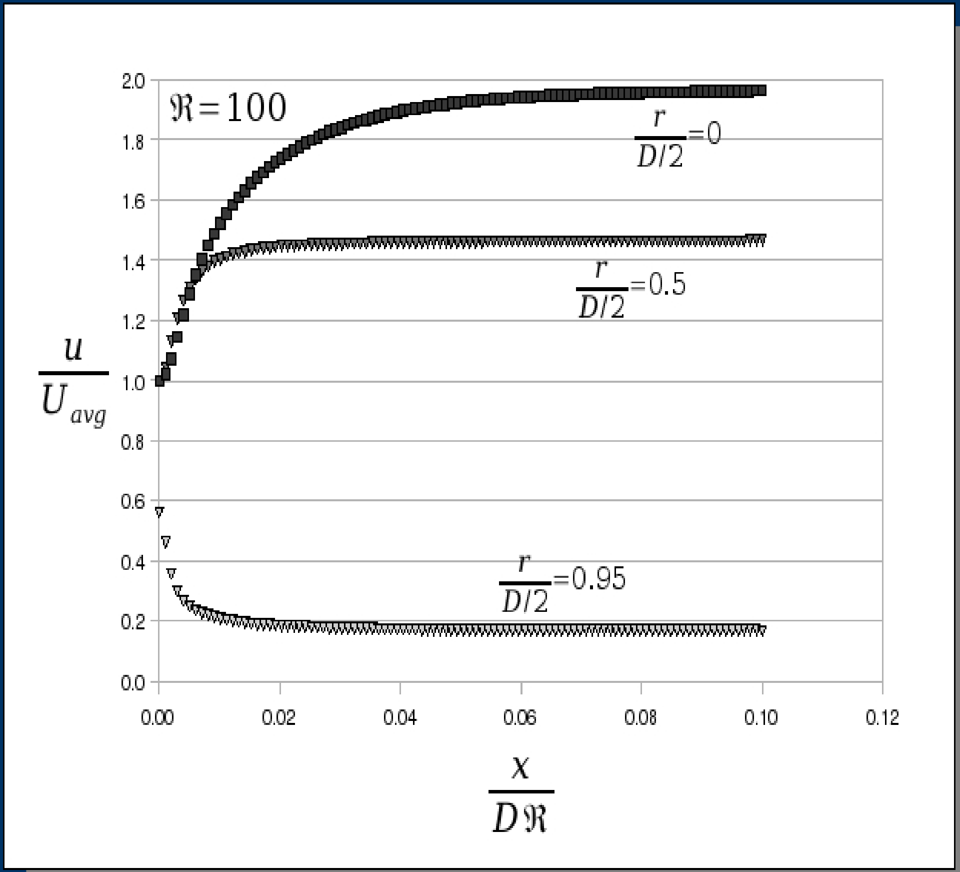
Entrance Length in Microtubes

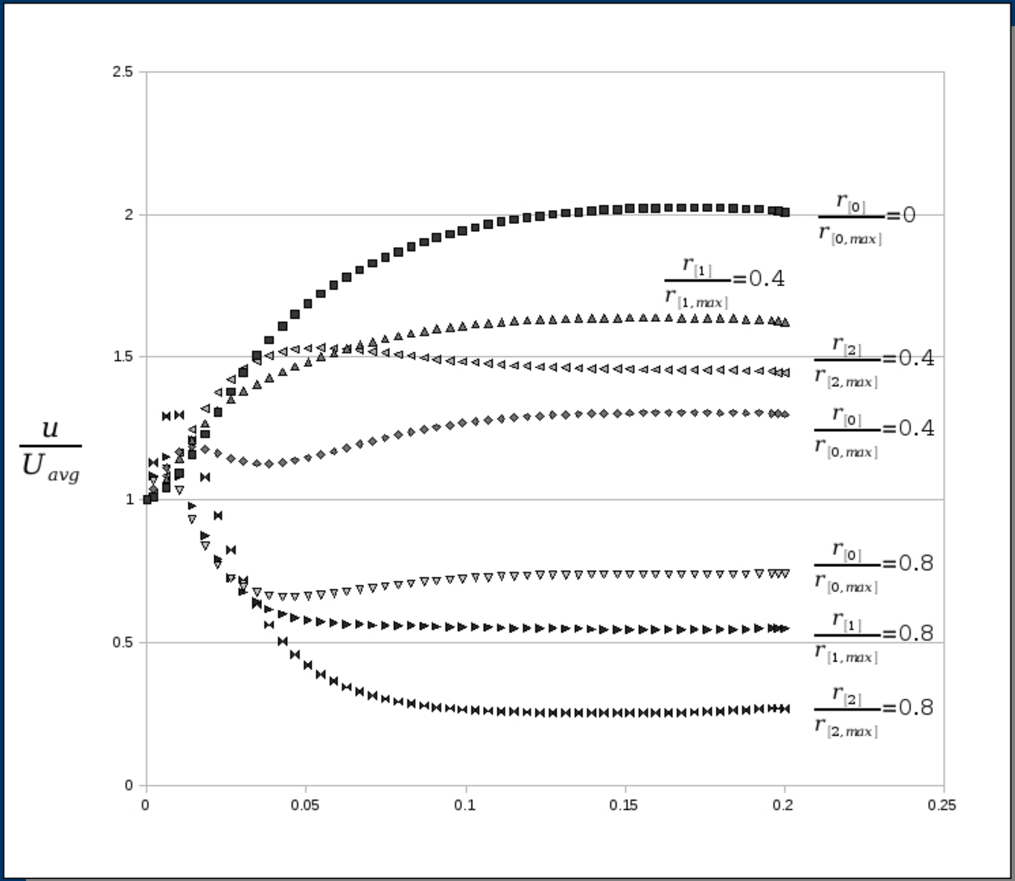


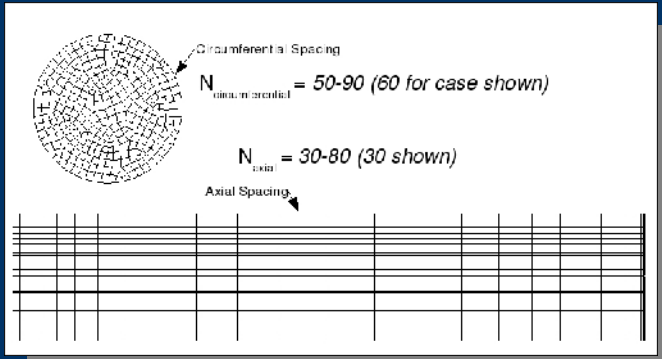


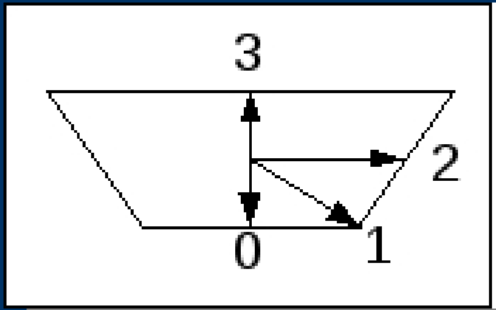


Entrance Length Results

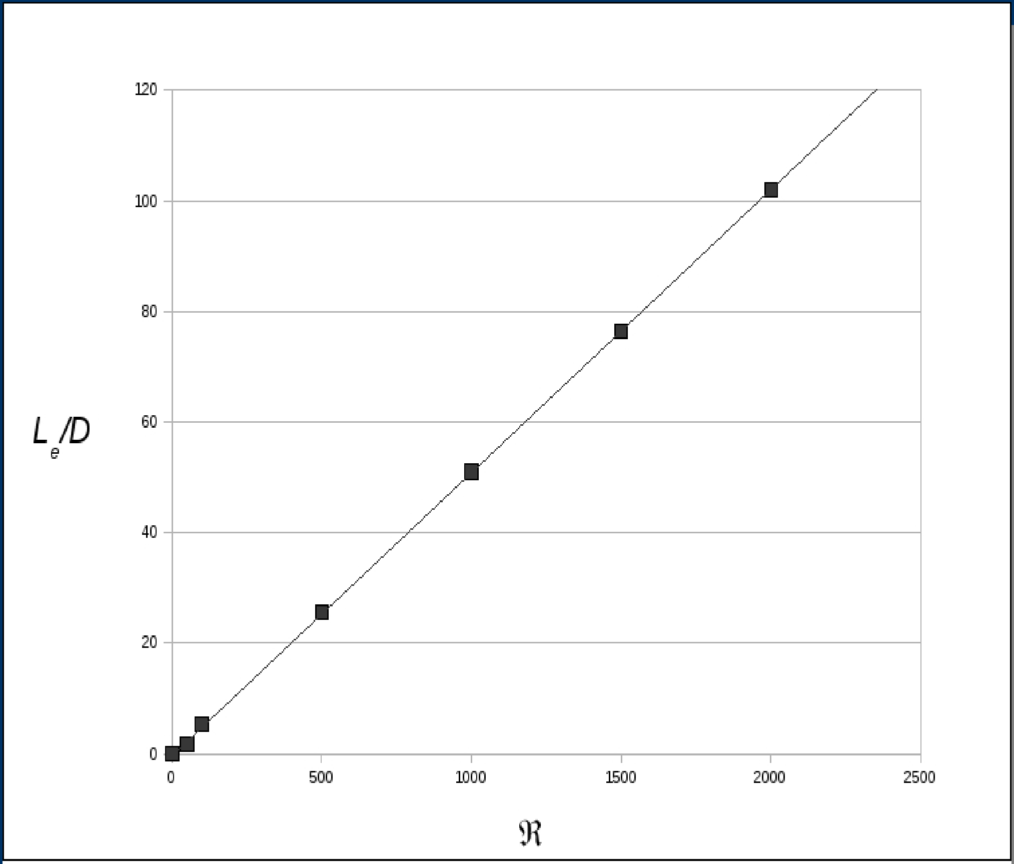


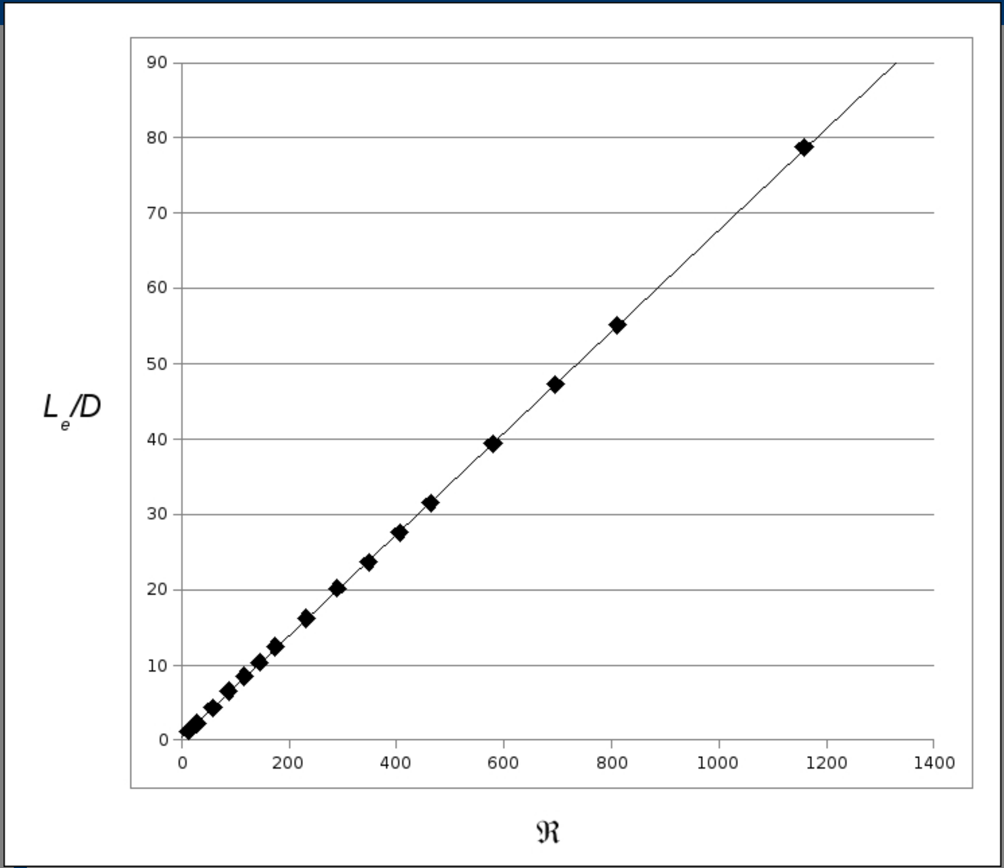




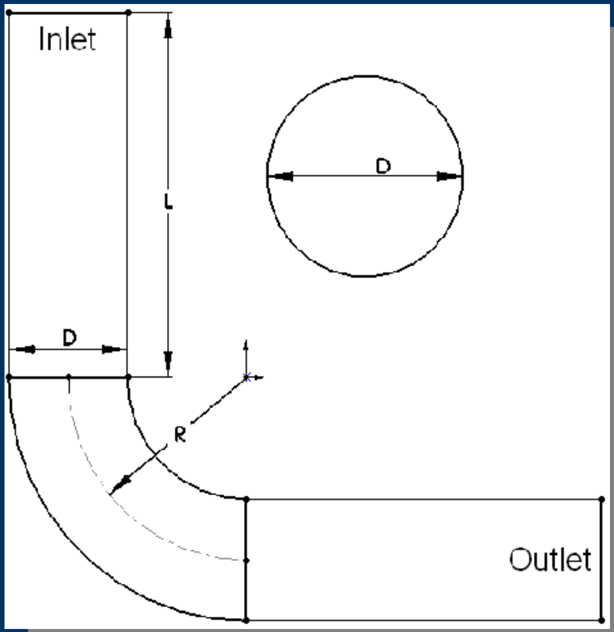


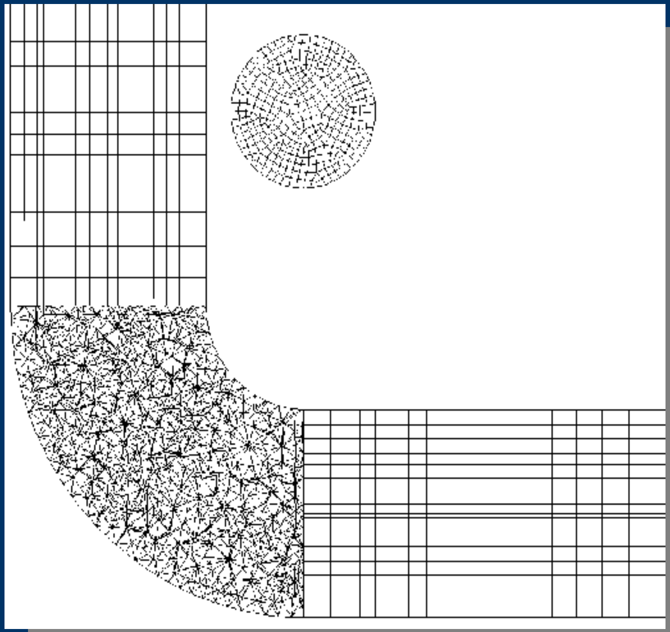
Entrance Length Results

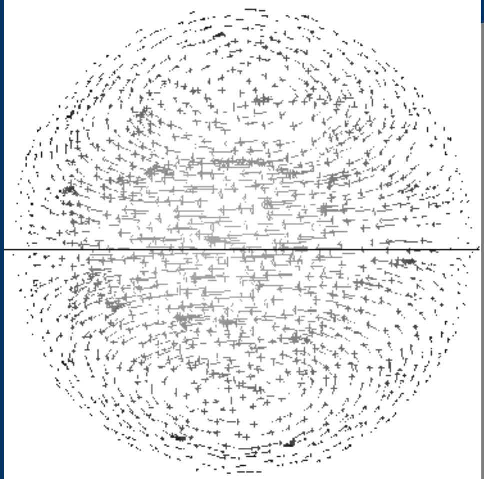


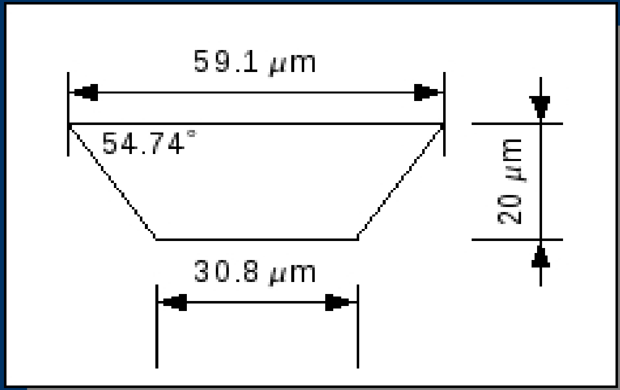


Loss Coefficients in Microelbows



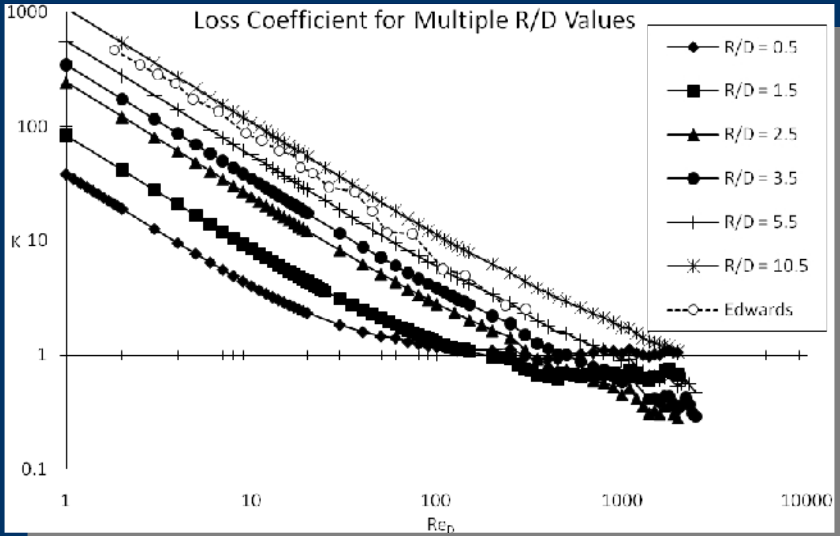




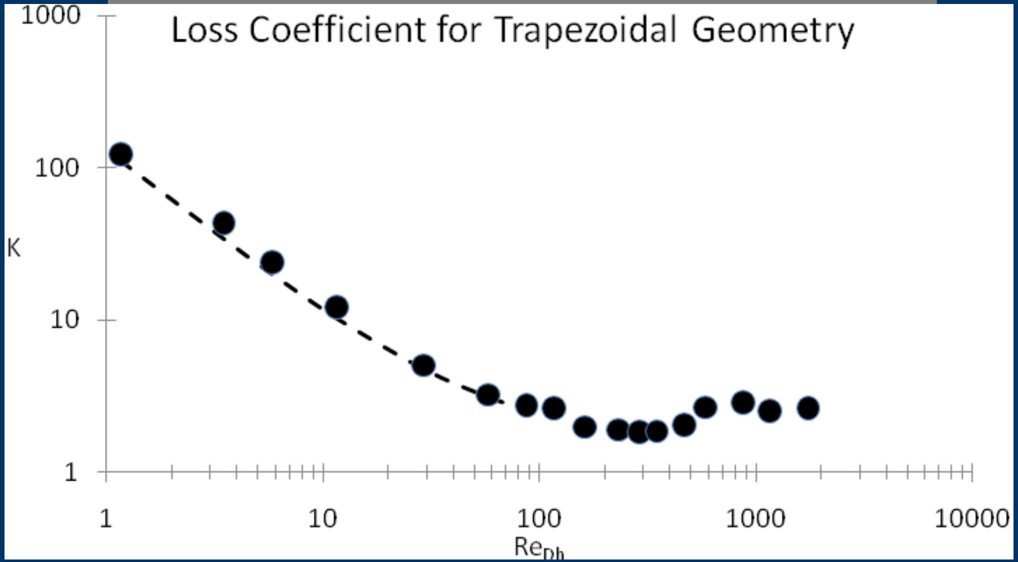


$$K = \frac{\Delta p}{\frac{1}{2}\rho V^2}$$

Microelbow Loss Coefficients



$$K = \frac{\Delta p}{\frac{1}{2}\rho V^2}$$



Millijunction Experiments

DESIGN & PRODUCTION

Objectives:

✓Design improved sealing method for part and increase re-usability of parts
✓Test the new designs
✓Document the production process

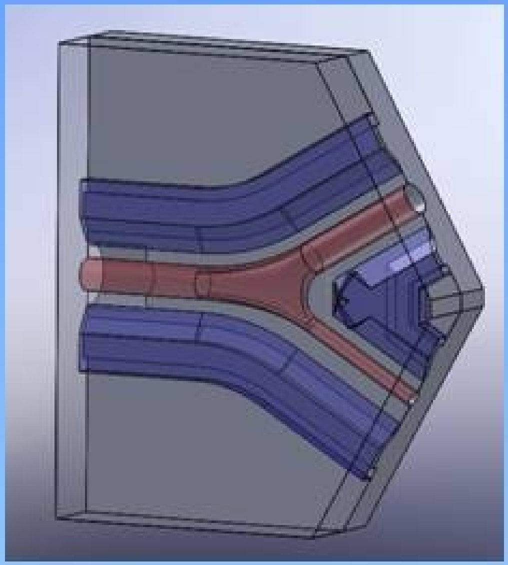
New Seal Design

We needed a seal design that would be leak-free and allow for quick and easy assembly and re-usability. The chosen design is loosely based on fuel injector seals.

New tap blocks were milled to allow for flexibility in pressure tap placement. By adapting the smaller OD tubing to ½″ we can use one block design for multiple sizes of tubing. The left is the inlet block and the right is the 1/8″ outlet.

Two o′rings are placed on the ends of each connecting pipe downstream from the head tank.

The existing flow straightener was reused by manufacturing an adapter that converted the threaded end to the new o′ring type. This design has the advantage that there is no time spent waiting for sealant to dry so parts can be swapped out with no down time.



Here is the Solidworks model as well as the physical realization of our efforts to create a useable bifurcation.

Upstream from the head tank and downstream from the junction are our new, highly sensitive needle valves used to adjust the head tank flow and the flow fraction through the bifurcation.

The flow straightener we designed has a replaceable core made of glass micropipettes that can be removed completely for unrestricted flow.

Data Acquisition

Jesse Haubrich

Collecting Data

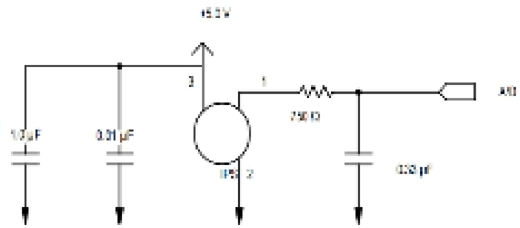
Sensor

- Submersible
- Internal Instrumentation Op-Amp

MPVZ5004GW7U
CASE 1560-02

Filter

- 750Hz Low Pass
- Reduces Noise from 10mV to 2mV

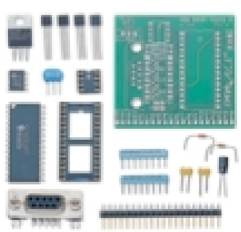


ADC

- 12 bit
- 11 Channel

Basic Stamp

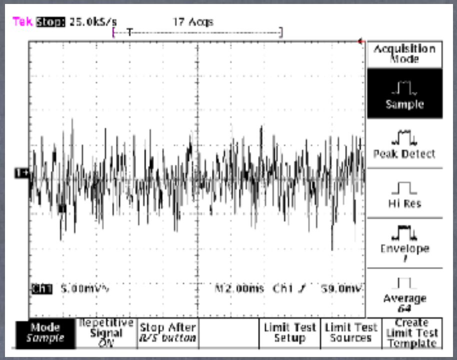
- Easy to program
- Affordable

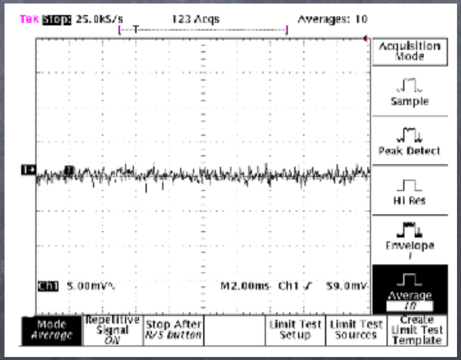


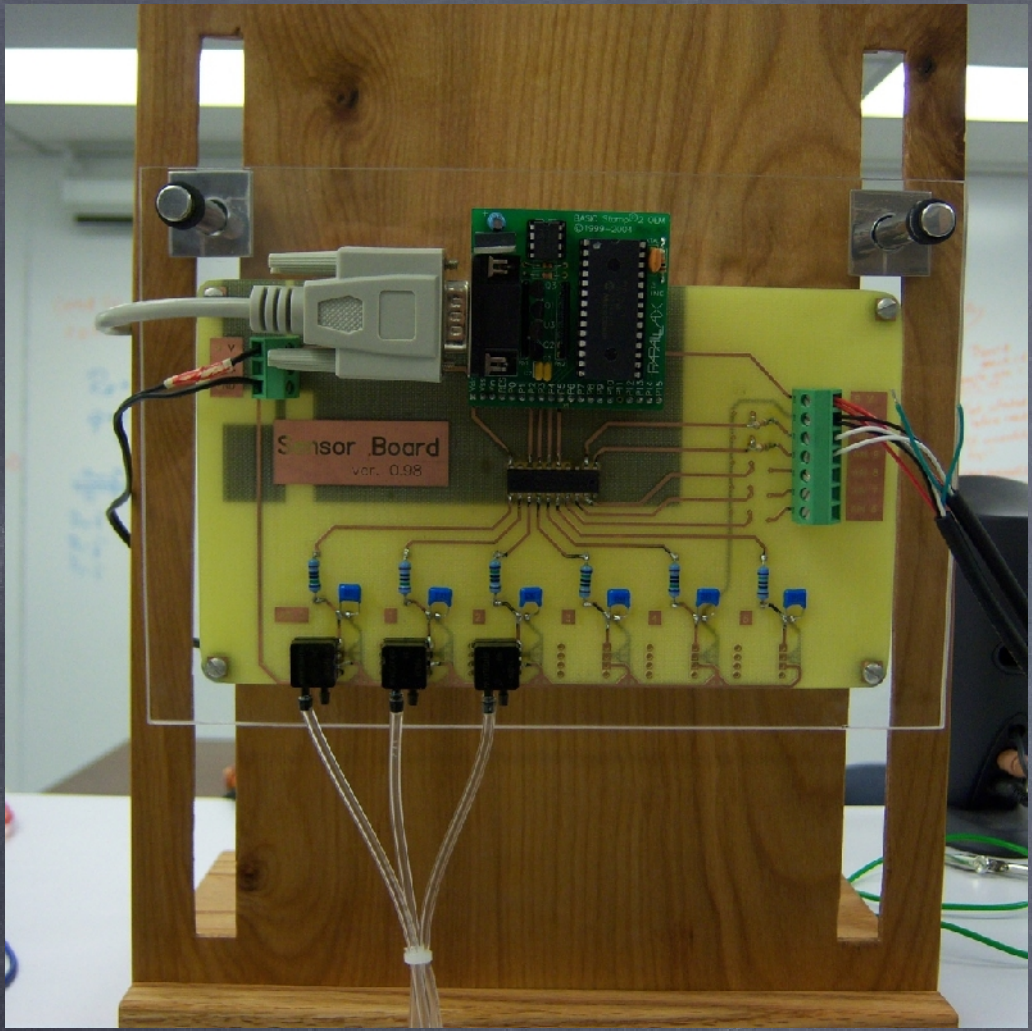
Computer

- Python
- Real Time Plotting with GNU Plot

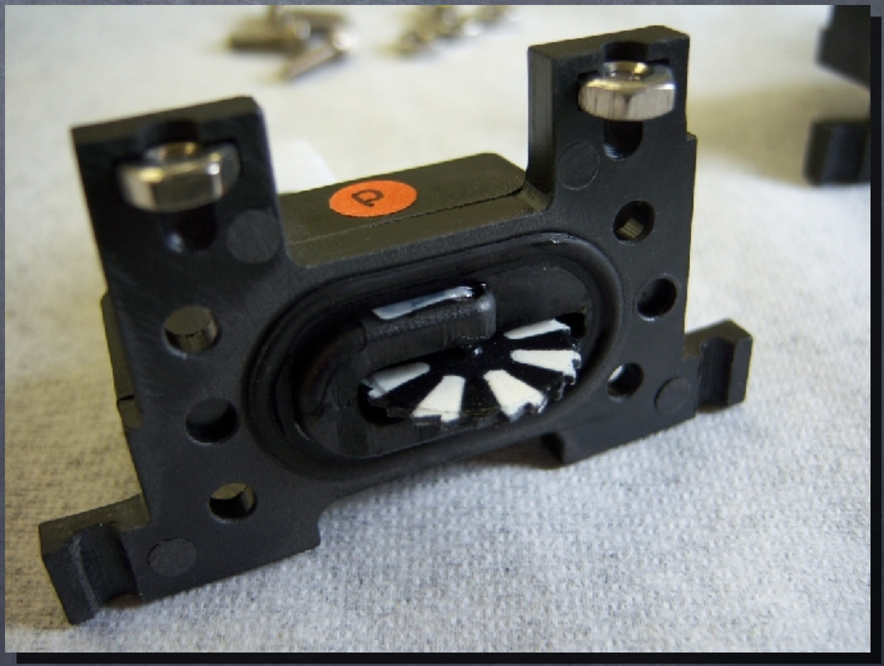
```
if __name__ == '__main__':
    serial = connect_serial()
    filesave = csv.writer(open("data.csv", "wb"))
    while True:
        data = serial.readline().split()
        filesave.writerow(data)
        plot(data)
```



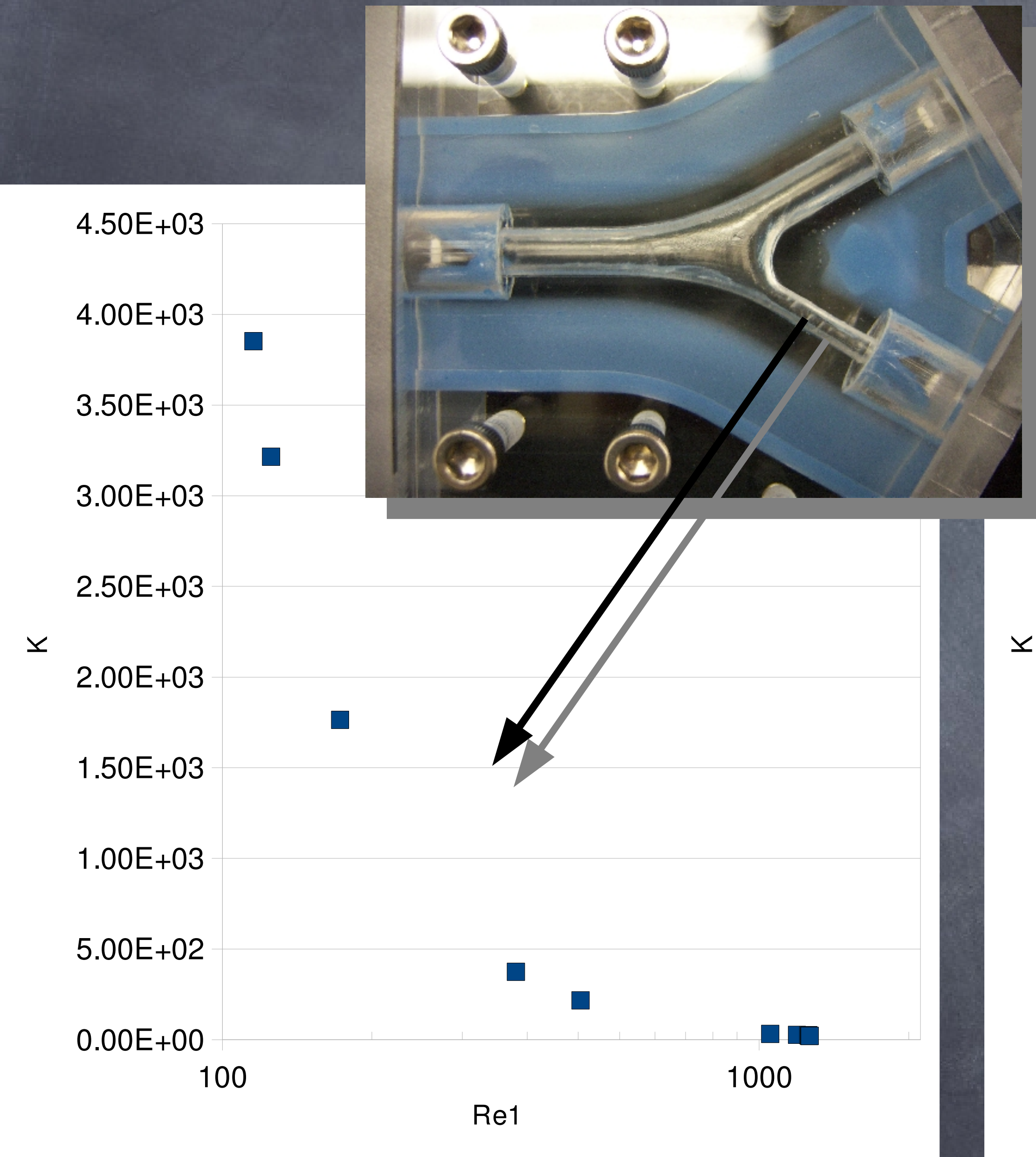


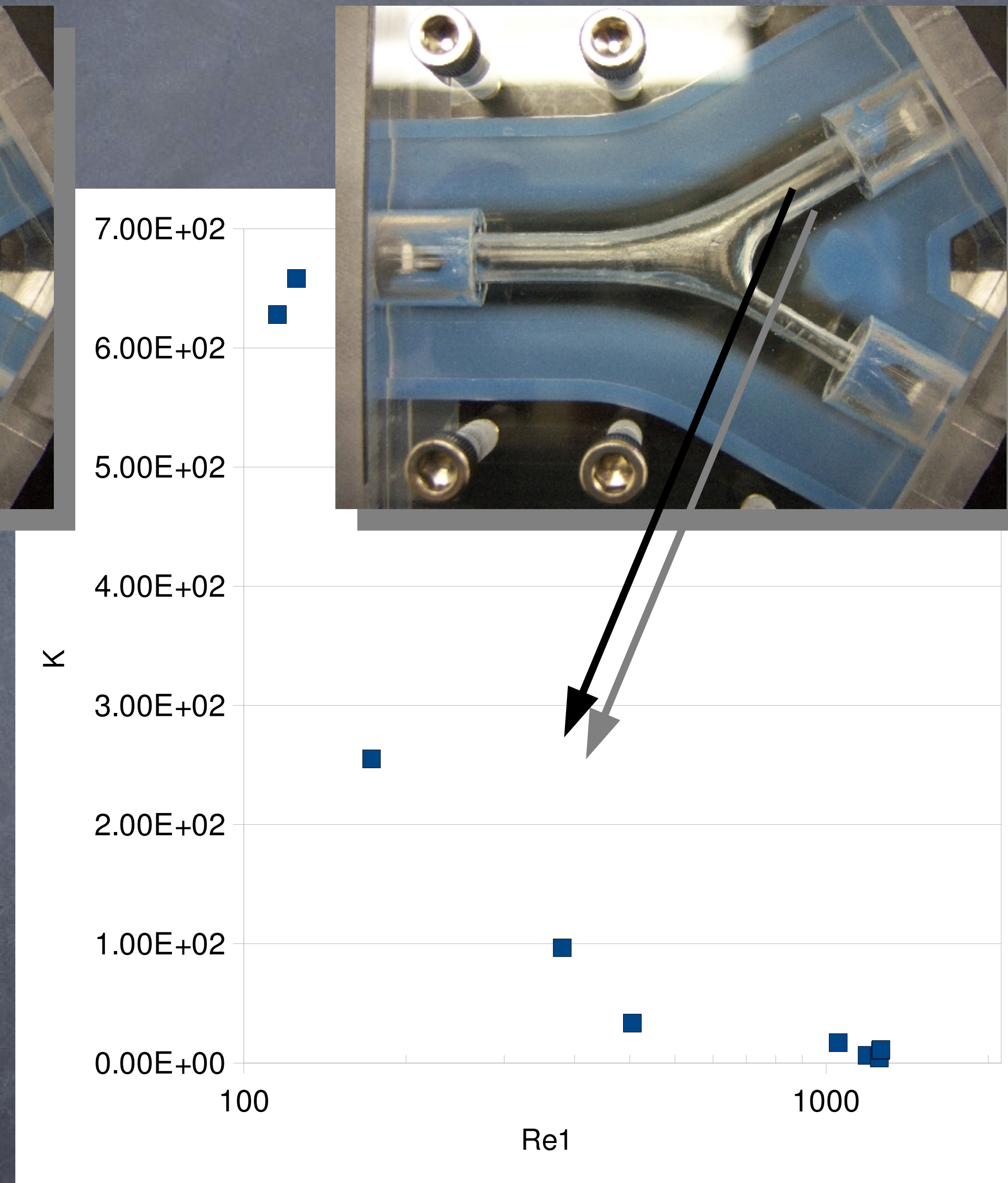


Basic Stamp
Passive Filter
Pressure Sensors
Flow Sensors
Python Interface



Loss Coefficient Experimental Results





Using Network Simulations to Understand Non-Darcy Flow

Objectives

Develop an algorithm to create, mesh, and perform CFD on simplified models of real porous media networks.

Equal number of entry and exit pores (no splits)

90° elbows only

No overlap of pores within media

Compare results of CFD to FTPM and empirical data in literature.

Modify algorithm to allow for complex models of real porous media.

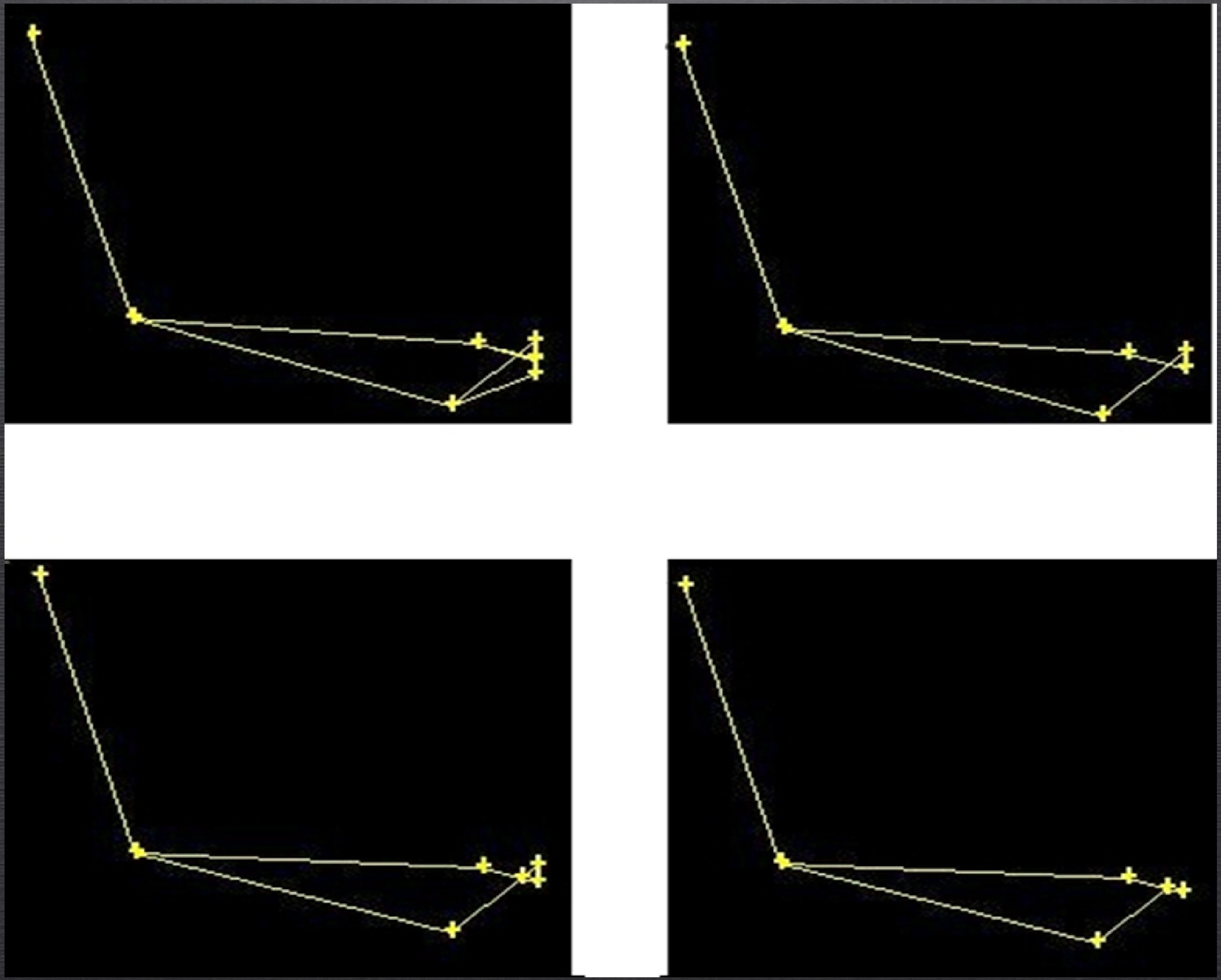
Splits with arbitrary angles

Overlaps

Using Network Simulations to Understand Non-Darcy Flow

Implementation of Objectives

Use custom codes to extract FTPM networks from code

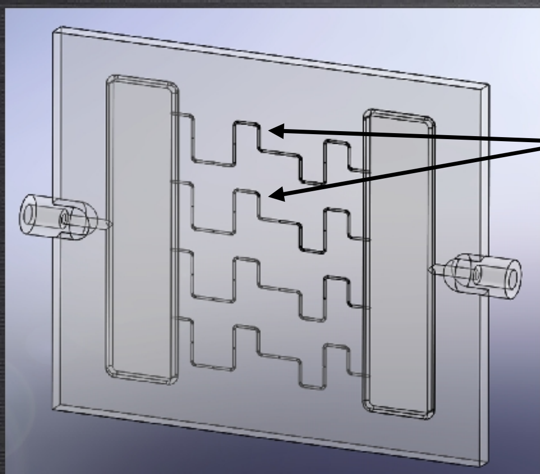


Using Network Simulations to Understand Non-Darcy Flow

Implementation of Objectives

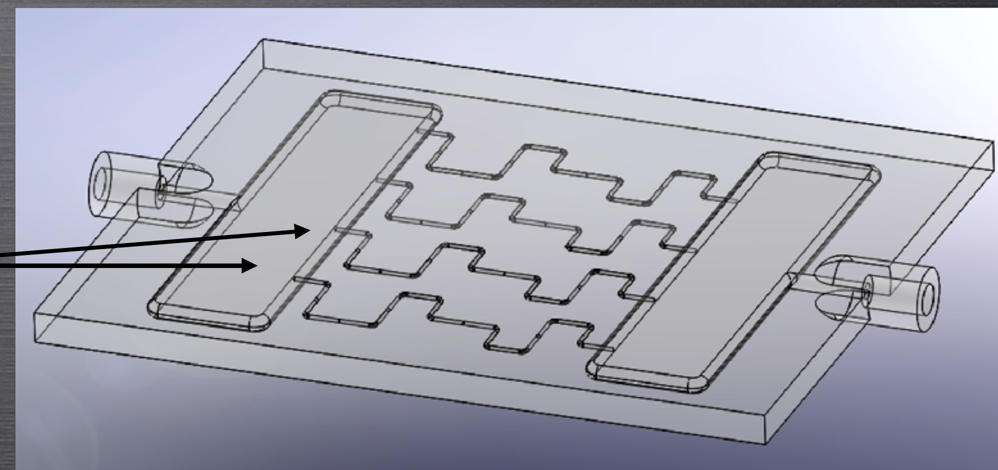
Use Solidworks to create network designs

Phase 1



90° elbows

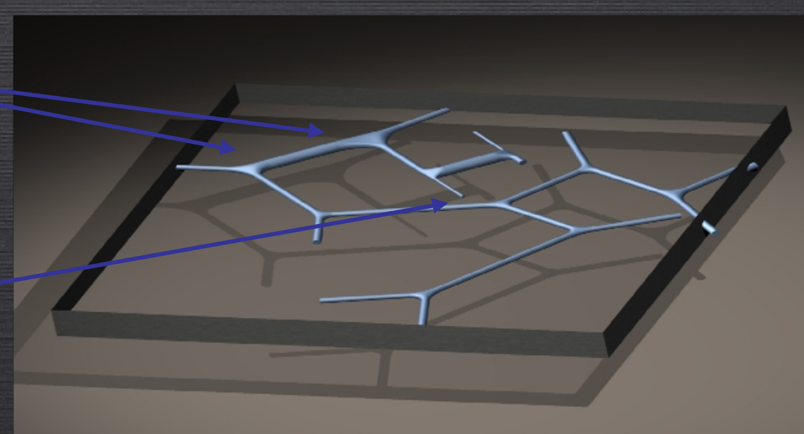
No overlapping



Phase 2

Arbitrary angles

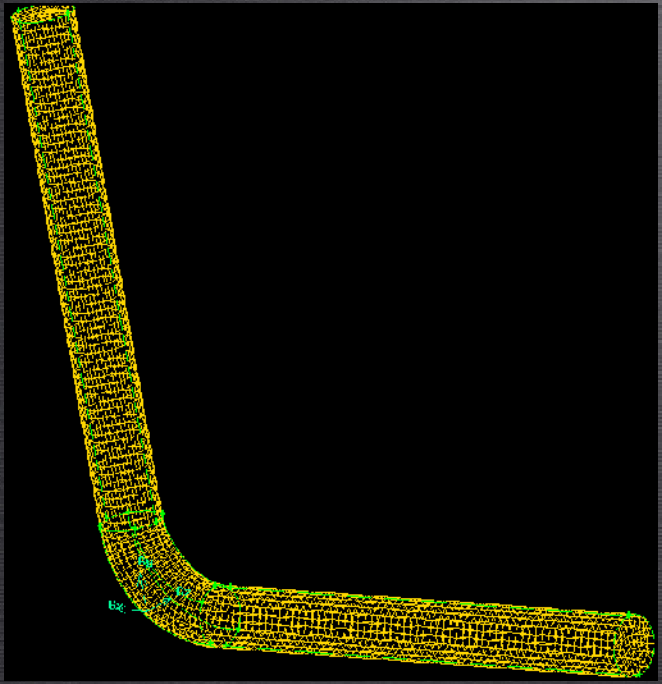
Possible overlaps



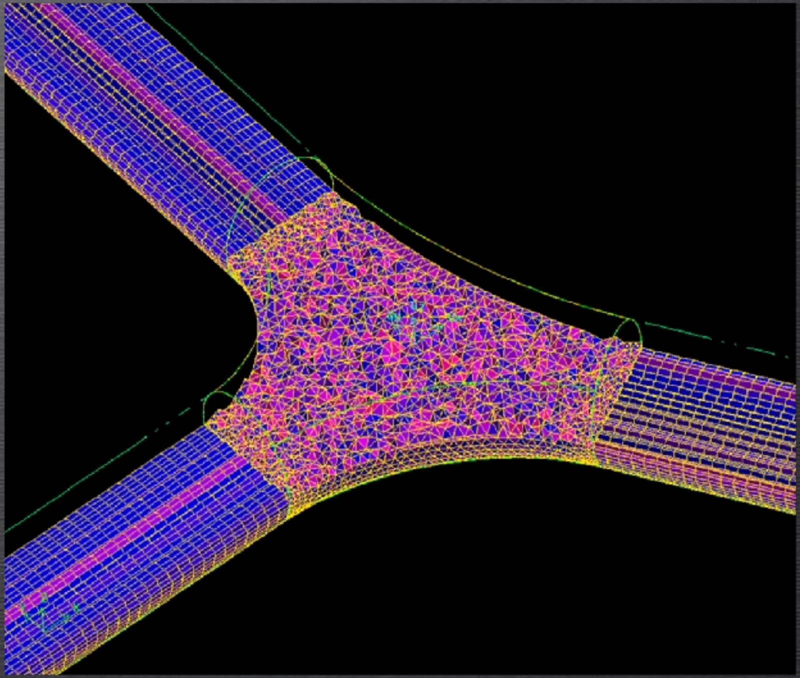
Using Network Simulations to Understand Non-Darcy Flow

Implementation of Objectives

Use Gambit to mesh networks



Close up of 90° elbow

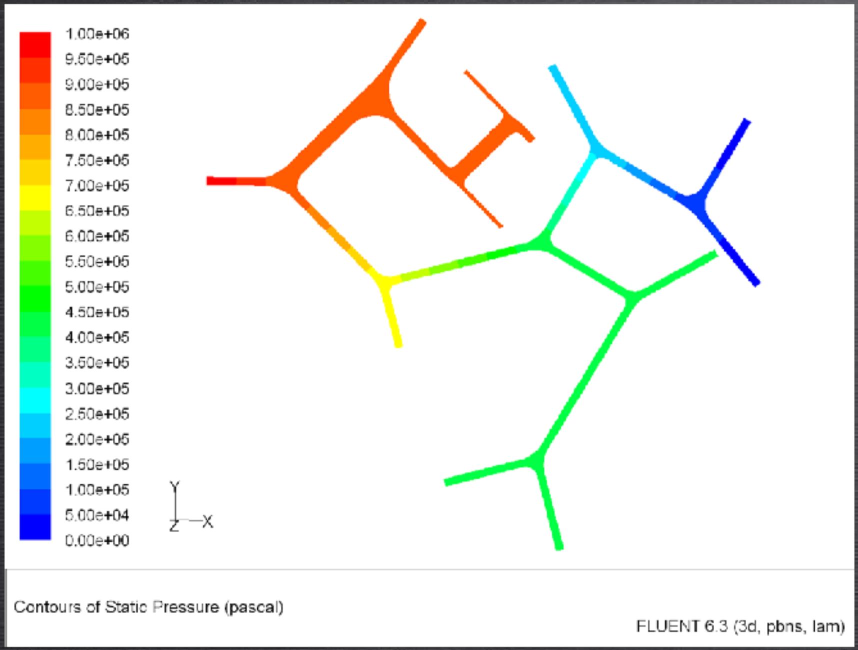


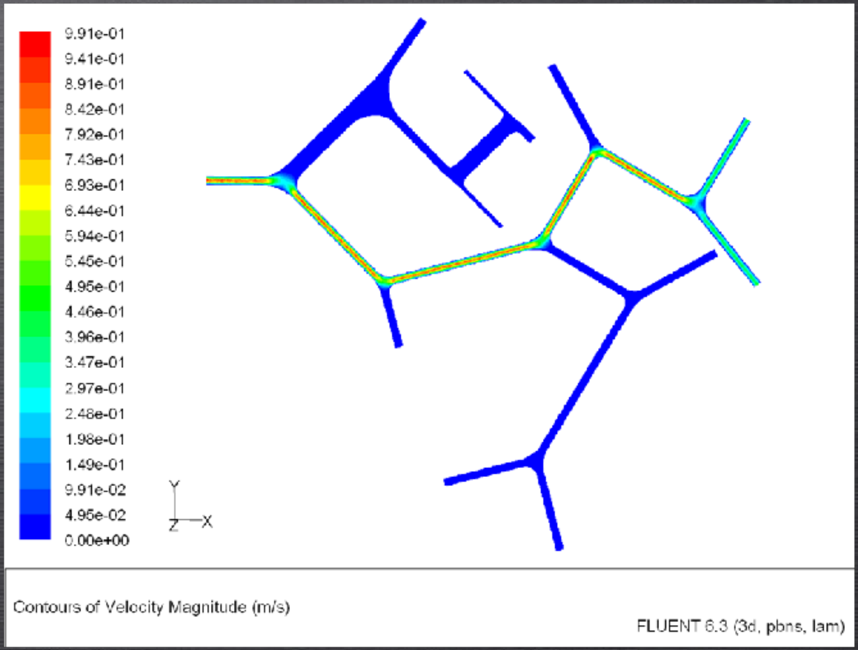
Close up of arbitrary junction

Using Network Simulations to Understand Non-Darcy Flow

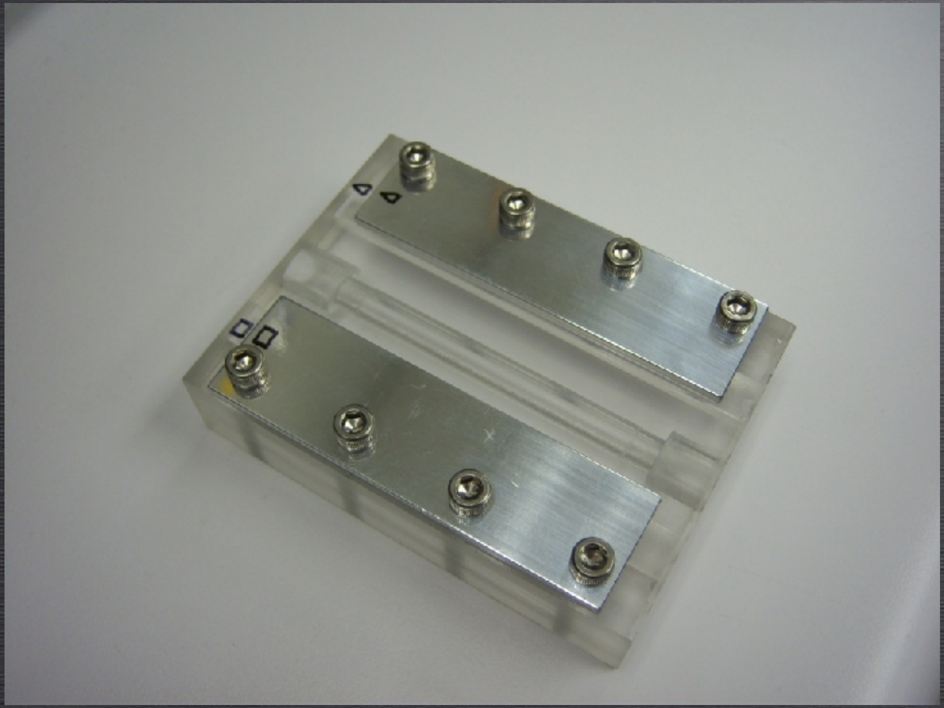
Implementation of Objectives

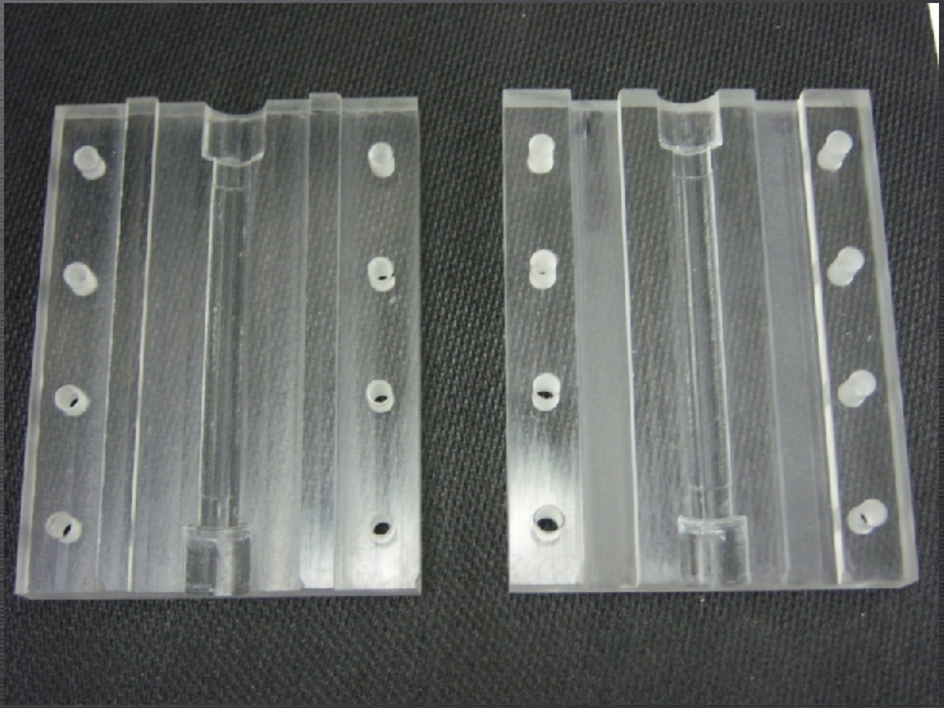
Use Fluent (CFD) to obtain κ and β from pressure and velocity data



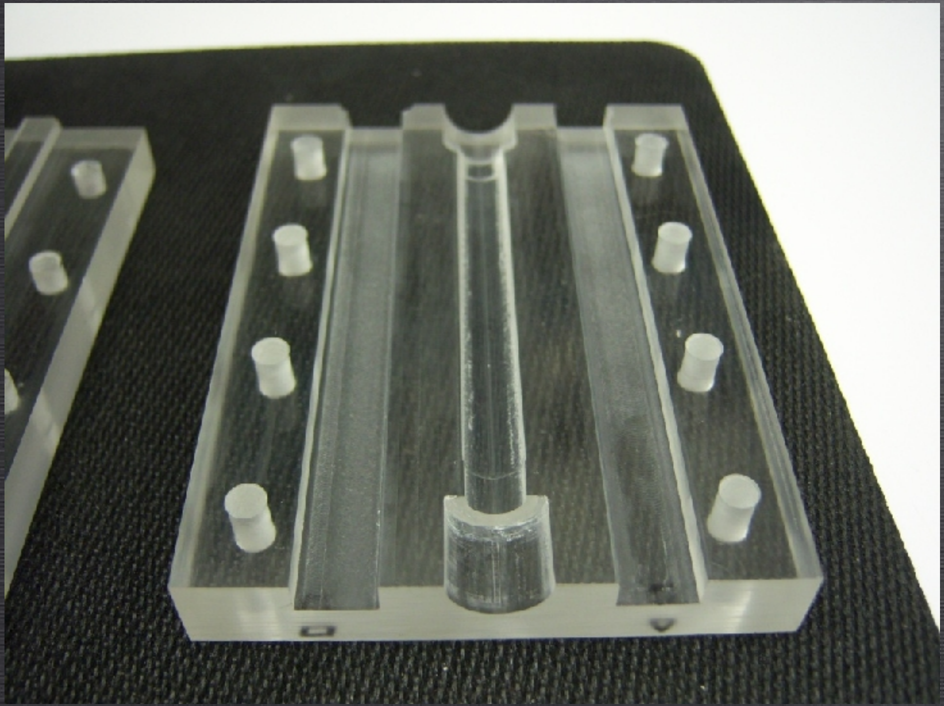


Bio-Scaffold Testing

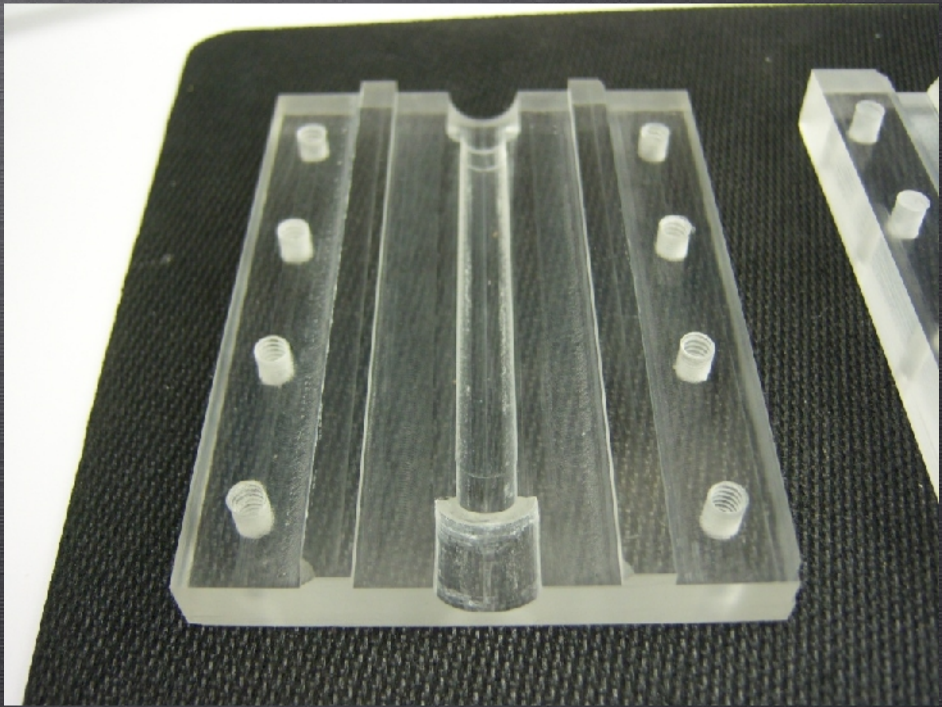




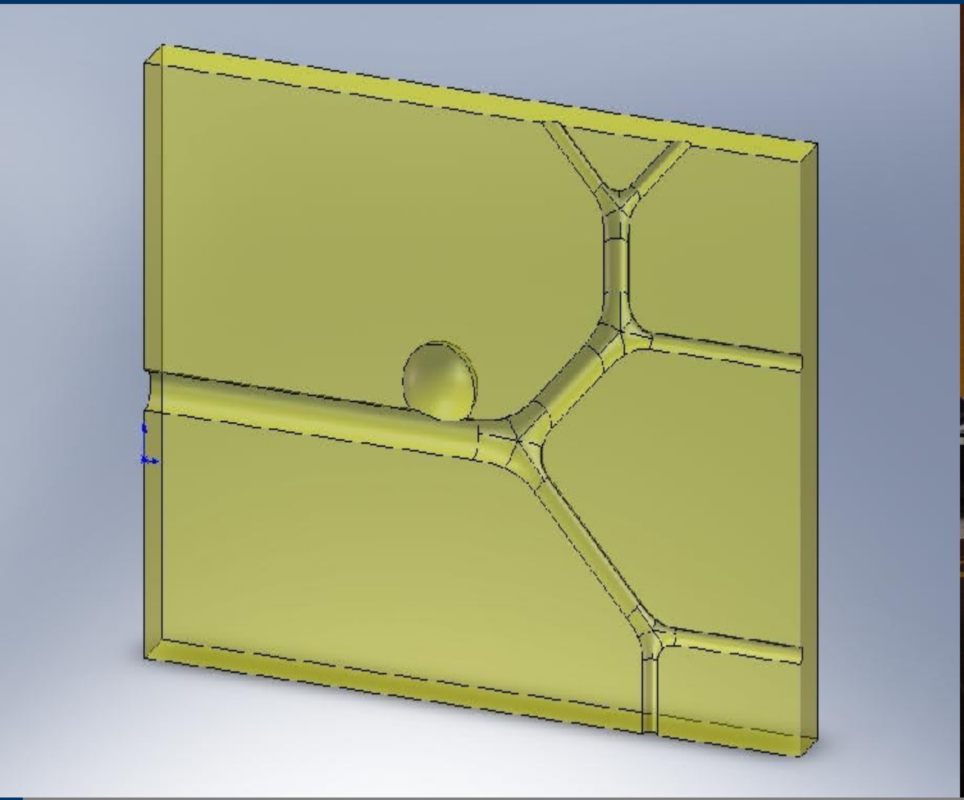
Top

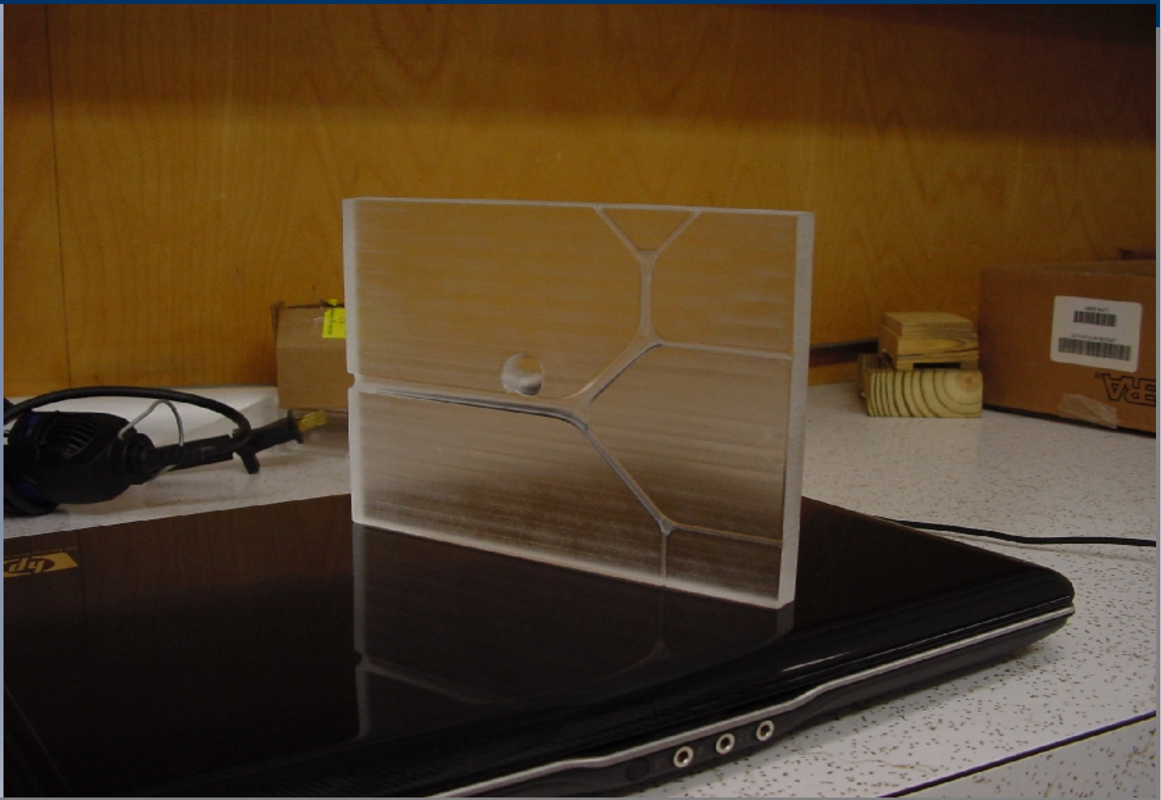


Bottom



Renal Artery Aneurysm Experiments





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